# ADVANCED MATERIALS

Selective recognition and dense packing of SO<sub>2</sub> clusters is achieved through multiple synergistic host-guest/guest-guest interactions within SiF<sub>6</sub><sup>2-</sup> anion-pillared hybrid porous materials in article number 1606929, by Qiwei Yang, Banglin Chen, Huabin Xing, and co-workers. The binding sites of anions and aromatic rings on the pore surface grasp every atom of SO<sub>2</sub> via S<sup> $\delta$ +...F<sup> $\delta$ -</sup> and O<sup> $\delta$ -...H<sup> $\delta$ +</sup> interactions, while the interactions between SO<sub>2</sub> molecules further promote the gas trapping.</sup></sup>

GAS PURIFICATION

Gas Purification



## Ultrahigh and Selective SO<sub>2</sub> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials

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The efficient capture of SO<sub>2</sub> is of great significance in gas-purification processes including flue-gas desulfurization and natural-gas purification, but the design of porous materials with high adsorption capacity and selectivity of SO<sub>2</sub> remains very challenging. Herein, the selective recognition and dense packing of SO<sub>2</sub> clusters through multiple synergistic host-guest and guestguest interactions by controlling the pore chemistry and size in inorganic anion (SiF<sub>6</sub><sup>2-</sup>, SIFSIX) pillared metal-organic frameworks is reported. The binding sites of anions and aromatic rings in SIFSIX materials grasp every atom of SO<sub>2</sub> firmly via S<sup> $\delta+\dots$ </sup> F<sup> $\delta-$ </sup> electrostatic interactions and O<sup> $\delta-\dots$ </sup> H<sup> $\delta+$ </sup> dipole-dipole interactions, while the guest-guest interactions between SO<sub>2</sub> molecules further promote gas trapping within the pore space, which is elucidated by first-principles density functional theory calculations and powder X-ray diffraction experiments. These interactions afford new benchmarks for the highly efficient removal of SO<sub>2</sub> from other gases, even if at a very low SO<sub>2</sub> concentration. Exceptionally high SO<sub>2</sub> capacity of 11.01 mmol g<sup>-1</sup> is achieved at atmosphere pressure by SIFSIX-1-Cu, and unprecedented low-pressure SO<sub>2</sub> capacity is obtained in SIFSIX-2-Cu-i (4.16 mmol g<sup>-1</sup> SO<sub>2</sub> at 0.01 bar and 2.31 mmol  $g^{-1}$  at 0.002 bar). More importantly, record SO<sub>2</sub>/ CO<sub>2</sub> selectivity (86-89) and excellent SO<sub>2</sub>/N<sub>2</sub> selectivity (1285-3145) are also achieved. Experimental breakthrough curves further demonstrate the excellent performance of these hybrid porous materials in removing lowconcentration SO<sub>2</sub>.

of low-grade fossil fuels.<sup>[3-6]</sup> Besides the direct detriment on environment and human health, SO2 will significantly inactivate the adsorbents or absorbents in removing CO<sub>2</sub> from flue gas although the concentration of SO<sub>2</sub> in flue gas is very low (cat. 2000 ppm).<sup>[7,8]</sup> Moreover, in the reactions such as selective catalytic reduction of NO<sub>x</sub> and catalytic combustion of CH<sub>4</sub>,<sup>[9,10]</sup> even trace amount of SO<sub>2</sub> could poison the catalysts and this deactivation is irreversible. The traditional flue-gas desulfurization (FGD) processes, with limestone or organic solvents as the absorbents,<sup>[11,12]</sup> can remove about 90–95% SO<sub>2</sub>. However, these FGD technologies are energy-intensive and not efficient for the deep desulfurization. Therefore, there is an urgent demand for efficient technology to remove trace SO<sub>2</sub> in flue gas and other SO<sub>2</sub>-containing gases.

In the past decades, the development of energy-efficient physical-adsorption separation technology shows great potential in gas separation, which greatly motivates the design and synthesis of highly efficient porous materials.<sup>[13–15]</sup> Metal–organic frameworks (MOFs) and/ or porous coordination polymers are

Rapid economic growth all over the world has resulted in the excessive energy consumption as well as increasing environmental burdens.<sup>[1,2]</sup> One of the most serious related problems is the emission of sulfur dioxide (SO<sub>2</sub>), induced by the utilization

a class of hybrid porous materials composed of metal units joined by organic/inorganic linkers, in which the diversity of the organic/inorganic linkers and exquisite control over pore aperture size promise great potential for gas separation and purification.<sup>[16–18]</sup> However, compared to the separation of CO<sub>2</sub>

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and hydrocarbons,<sup>[19–29]</sup> the selective adsorption of SO<sub>2</sub> has rarely been studied on MOFs, especially the adsorption at low partial pressures that is actually needed by the gas desulfurization.<sup>[30–36]</sup> Generally, the desulfurization of flue gas is a step before CO<sub>2</sub> scrubbing process, however, few work paid attention to the selective removal of SO<sub>2</sub> from CO<sub>2</sub>. In fact, considering the acidic nature of both SO<sub>2</sub> and CO<sub>2</sub> molecules and the much lower SO<sub>2</sub> concentration in flue gas than CO<sub>2</sub> (CO<sub>2</sub>: 10–12%, v/v; SO<sub>2</sub>: about 2000 ppm), it is very challenging to remove SO<sub>2</sub> from CO<sub>2</sub> with high selectivity.<sup>[37,38]</sup> These abovementioned problems prompted us to develop advanced porous materials with delicate structure and chemistry for the adsorption of SO<sub>2</sub>, and elucidate the way in which contributions such as pore size and pore surface electrostatic environment enhance the selective recognition of SO<sub>2</sub> with high uptake capacity.

In this work, we for the first time reported the selective recognition and dense packing of the so-called "SO<sub>2</sub> cluster" using hybrid porous materials through precisely tuning the pore size and pore chemistry. Featuring copper coordination networks with inorganic hexafluorosilicate (SiF<sub>6</sub><sup>2-</sup>, SIFSIX) anions and organic linkers, SIFSIX-1-Cu  $(1 = 4,4'-bipyridine)^{[24]}$ and SIFSIX-2-Cu-i (2 = 4,4'-dipyridylacetylene, i = interpenetrated)<sup>[19]</sup> contain pore spaces that enable high SO<sub>2</sub> uptake with specific recognition and afford new benchmarks for the highly efficient removal of SO<sub>2</sub> from other gases. Not only extraordinary ambient uptake of SO2 was achieved with SIFSIX-1-Cu as adsorbent, but also unprecedented low-pressure SO2 capacity was attained with SIFSIX-2-Cu-i. Moreover, record SO<sub>2</sub>/CO<sub>2</sub> selectivity and excellent SO<sub>2</sub>/N<sub>2</sub> selectivity were also exhibited by the SIFSIX materials. We attribute this exceptional performance to the synergistic guest–host interactions ( $S^{\delta+} \cdots F^{\delta-}$  and  $O^{\delta-}\cdots H^{\delta+}$  interactions) that firmly grasp every atom of  $SO_2$ in the pores of SIFSIX materials along with the considerable guest-guest interactions among SO2 molecules and the optimal pore size, which together enable the preferential binding and cluster formation of  $SO_2$  in the pores densely.

These SIFSIX materials exhibit a pillared square-grid 3D structure with inorganic SiF<sub>6</sub><sup>2-</sup> ions as a linear bridge between transition-metal moieties. Previously, we have succeeded in the specific recognition of acetylene from ethylene using SIFSIX materials.<sup>[39]</sup> In this work, we systematically studied the adsorption of SO2 on SIFSIX-1-Cu, SIFSIX-2-Cu (2, 4,4'-dipyridylacetylene), SIFSIX-2-Cu-i, SIFSIX-3-Zn (3,pyrazine), and SIFSIX-3-Ni at atmospheric and low pressures. At first, the uptake capacity of SO2 as single-component gas on activated SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were determined at 298 K and 1.01 bar (Table 1). Remarkably, SIFSIX-1-Cu exhibited superb adsorption capacity (11.01 mmol g<sup>-1</sup>) among SIFSIX materials, while SIFSIX-2-Cu-i and SIFSIX-2-Cu uptake 6.90 and 6.50 mmol g<sup>-1</sup>, respectively (Table 1). To the best of our knowledge, this extraordinarily high value of 11.01 mmol g<sup>-1</sup> measured at room temperature and ambient pressure is the highest of all the materials reported under the same condition so far, including top-performing ones such as M(bdc)(ted)<sub>0.5</sub> (9.97 mmol g<sup>-1</sup>),<sup>[36]</sup> NOTT-300 (Al) (7.1 mmol g<sup>-1</sup>),<sup>[34]</sup> MFM-300(In) (8.28 mmol g<sup>-1</sup>),<sup>[35]</sup> and MFM-202a (10.2 mmol g<sup>-1</sup>).<sup>[33]</sup>

The adsorption isotherms of SO<sub>2</sub> at 298 and 273 K on SIFSIX materials were measured to systematically demonstrate the SO<sub>2</sub> capture ability of these materials at low pressures (Figure 1 and Table 1), as needed by the actual desulfurization process due to the low SO<sub>2</sub> concentration in feed gas. Notably, the measurements were performed using SO<sub>2</sub>/N<sub>2</sub> mixed gas with varying SO<sub>2</sub> molar fractions under flow mode.

As can be noted from Figure 1A, the adsorption isotherms of  $SO_2$  on SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Ni, and SIFSIX-3-Zn show a steep increase in the low-pressure range and then reach saturation. At an extremely low  $SO_2$  partial pressure of

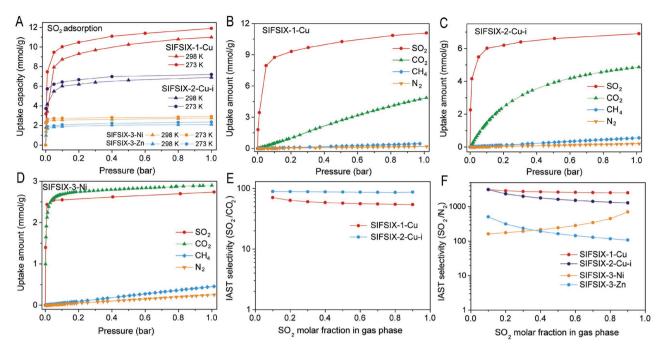
**Table 1.** The adsorption capacities of  $SO_2$  in various porous materials at different partial pressure of  $SO_2$ . Summary of the adsorption collected at 298 K. Note: The  $SO_2$  adsorption capacities at 0.002, 0.01, and 0.1 bar were determined using  $SO_2/N_2$  mixed gas with varying  $SO_2$  molar fractions under flow mode, while the  $SO_2$  adsorption capacities at 1.0 bar were determined using  $SO_2$  pure gas.

Materials			uptake ol g <sup>-1</sup> ]		Selectivity for SO <sub>2</sub> /CO <sub>2</sub> at 10/90 mixture	Selectivity for SO <sub>2</sub> /N <sub>2</sub> Selectivity for SO <sub>2</sub> /CH <sub>4</sub> at 10/90 mixture at 10/90 mixture	Q <sub>st</sub> [SO <sub>2</sub> kJ mol <sup>-1</sup> ]	
	0.002 bar <sup>a)</sup>	0.01 bar <sup>a)</sup>	0.1 bar <sup>a)</sup>	1.0 bar				
SIFSIX-1-Cu	1.80	3.43	8.74	11.01	70.7	3145.7	1241.4	36.1
SIFSIX-2-Cu-i	2.31	4.16	6.01	6.90	87.1	3103.2	1017.1	38.1
SIFSIX-3-Zn	0.98	1.68	1.89	2.10	_	506.7	276.0	45.2
SIFSIX-3-Ni	1.39	2.43	2.55	2.74	_	701.8	371.6	43.2
SIFSIX-2-Cu	-	-	-	6.50	_	-	_	-
Ni(bdc) (ted) <sub>0.5</sub> <sup>[36]</sup>	-	-	3.50	9.97	_	-	_	-
Zn-MOF-74 <sup>[30]</sup>	-	3.03 <sup>b)</sup>	-	-	_	-	_	-
MFM-300(In) <sup>[35]</sup>	_	-	-	8.28	50 <sup>d</sup> )	2700 <sup>d)</sup>	_	34.5/39.6 <sup>e)</sup>
MFM-202a <sup>[33]</sup>	_	-	3.0	10.2	-	-	_	35
NOTT-300 (Al) <sup>[34]</sup>				7.1 <sup>f)</sup>				
P(TMGA-co-MBA) <sup>[40]</sup>	-	-	-	4.06	-	-	-	-
Activated Carbon <sup>[41]</sup>	_	-	_	3.3 <sup>c)</sup>	-	_	_	-

<sup>a)</sup>Partial pressure of SO<sub>2</sub>; <sup>b)</sup>Dynamic adsorption capacity; <sup>c)</sup>At the temperature of 323 K and pressure of 0.46 bar; <sup>d)</sup>These data were read from the figures of ref. [35]; <sup>e)</sup>Highest  $Q_{st}$  values at different surface coverage; <sup>f)</sup>At the temperature of 298 K.







**Figure 1.** A) SO<sub>2</sub> adsorption isotherms of SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni at 273 and 298 K. Adsorption isotherms for SO<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub> and N<sub>2</sub> on B) SIFSIX-1-Cu, C) SIFSIX-2-Cu-i, and D) SIFSIX-3-Ni at 298 K. Note: SO<sub>2</sub> isotherms were measured using SO<sub>2</sub>/N<sub>2</sub> mixed gas with varying SO<sub>2</sub> molar fractions under flow mode. CO<sub>2</sub>, CH<sub>4</sub> and N<sub>2</sub> isotherms were measured using single-component gas. IAST selectivities of SIFSIX materials with E) SO<sub>2</sub>/CO<sub>2</sub> mixtures and F) SO<sub>2</sub>/N<sub>2</sub> mixtures with varying SO<sub>2</sub> molar fractions in gas phase at 100 kPa.

0.002 bar (2000 ppm) and 298 K, SIFSIX-2-Cu-i rapidly uptake as high as 2.31 mmol g<sup>-1</sup> SO<sub>2</sub> (Figure 1C and Table 1), exceeding the capacity of SIFSIX-1-Cu (1.80 mmol g<sup>-1</sup>), SIFSIX-3-Zn (0.98 mmol  $g^{-1}$ ), and SIFSIX-3-Ni (1.39 mmol  $g^{-1}$ ) (Figure 1B,D and Table 1). This excellent capacity of SO2 at such a low pressure indicates that SIFSIX-2-Cu-i has great potential in FGD applications. At 298 K, when the partial pressure of SO<sub>2</sub> increased to 0.01 bar, the SO2 uptake of SIFSIX-2-Cu-i rose to 4.16 mmol  $g^{-1}$  SO<sub>2</sub>, not only still higher than the other three SIFSIX materials but also exceeding the benchmark uptake of Zn-MOF-74 (3.03 mmol  $g^{-1}$ ). As the pressure of SO<sub>2</sub> further increased to 0.1 bar, the uptake amount of SO<sub>2</sub> at 298 K on SIFSIX-1-Cu increased more rapidly and became more than that on SIFSIX-2-Cu-i, approaching a value of 8.74 mmol g<sup>-1</sup> while SIFSIX-2-Cu-i exhibits 6.01 mmol g<sup>-1</sup>, both higher than that ever reported under the same conditions (3.5 mmol  $g^{-1}$  by  $Ni(bdc)(ted)_{0.5}$ ). When the temperature decreased to 273 K, a steep increase in the low-pressure range of isotherms to a high SO<sub>2</sub> capacity was still observed on all these five SIFSIX materials. As shown in Figure 1A, at 273 K and the low SO<sub>2</sub> partial pressure of 0.002 bar, SIFSIX-2-Cu-i exhibited remarkable higher uptake of SO<sub>2</sub> (3.72 mmol g<sup>-1</sup>), exceeding SIFSIX-1-Cu (3.18 mmol  $g^{-1}$ ) and SIFSIX-3-Ni (2.34 mmol  $g^{-1}$ ). With the increase of SO<sub>2</sub> partial pressure, SIFSIX-1-Cu exhibited higher uptake than SIFSIX-2-Cu-i, SIFSIX-3-Ni, and SIFSIX-3-Zn within the whole range of 0.01-1.01 bar. Overall, the results in Table 1 and Figure 1A demonstrate that exceptional SO<sub>2</sub> capacity can be afforded by SIFSIX materials from atmospheric to very low pressures, even more superior at low pressures.

To evaluate the selectivity of  $SO_2$  to other typical gases in gas desulfurization processes, adsorption isotherms of  $CO_2$ ,  $CH_4$ ,

and N<sub>2</sub> on SIFSIX materials were collected at 298 K using pure gas. Although both CO<sub>2</sub> and SO<sub>2</sub> are acidic gases, the CO<sub>2</sub> isotherms on SIFSIX-1-Cu show dramatically different adsorption behaviors than SO<sub>2</sub> adsorption isotherms (Figure 1B,C). These dramatic differences between SO<sub>2</sub> and CO<sub>2</sub> adsorption behavior and capacity, especially at low pressures, offer a great potential of selective recognition of SO<sub>2</sub> toward CO<sub>2</sub> on SIFSIX-1-Cu and SIFSIX-2-Cu-i. In addition, SIFSIX-1-Cu and SIFSIX-2-Cu-i only adsorbed 0.45 and 0.55 mmol g<sup>-1</sup> CH<sub>4</sub> at 298 K and 1.0 bar (Figure 1A,B), respectively, which are negligible compared to SO<sub>2</sub> uptake capacity. Furthermore, the uptake amount of N<sub>2</sub> was much lower than CH<sub>4</sub> (Figure 1B–D). As for the case of SIFSIX-3-Ni (Figure 1D) and SIFSIX-3-Zn (Figure S4, supporting information), the CO<sub>2</sub> capacity was higher than the SO<sub>2</sub> capacity, and CH<sub>4</sub> and N<sub>2</sub> were still rarely adsorbed.

In order to further address the separation capability of SIFSIX materials in different gas desulfurization processes, SO<sub>2</sub>/CO<sub>2</sub> and SO<sub>2</sub>/N<sub>4</sub> separation selectivity were determined using ideal adsorbed solution theory (IAST) calculations as a function of varying  $SO_2$  composition (from 0.1 to 0.9).<sup>[42,43]</sup> Notably, in these IAST calculations, the SO<sub>2</sub> isotherms on SIFSIX materials were measured using SO<sub>2</sub>/N<sub>2</sub> mixed gas, which might slightly underestimate the selectivity. As shown in Figure 1E, SIFSIX-1-Cu shows excellent SO<sub>2</sub>/CO<sub>2</sub> separation selectivity (54-70) over a wide range of SO<sub>2</sub> molar fraction in gas phase (0.1–0.9), especially in the low concentration range. Even better, SIFSIX-2-Cu-i exhibits record SO<sub>2</sub>/CO<sub>2</sub> selectivity (86-89) within 0.1-0.9 molar fraction of SO<sub>2</sub>. Considering the fact of low SO<sub>2</sub> concentration in typical flue gas  $(SO_2/CO_2/N_2)$ , this large SO<sub>2</sub>/CO<sub>2</sub> selectivity endows SIFSIX-1-Cu and SIFSIX-2-Cu-i with potential in FGD process. This is crucial to realize

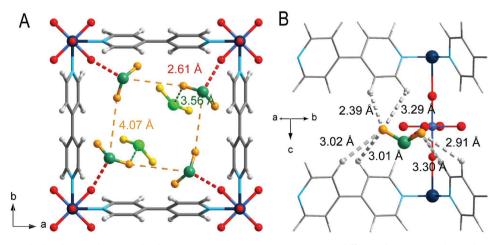


a thorough removal of trace SO<sub>2</sub> from flue gas before the CO<sub>2</sub> scrubbing process to ensure the activity of CO<sub>2</sub> adsorbent. To the best of our knowledge, the SO2/CO2 IAST selectivity on SIFSIX-2-Cu-i (86-89) and SIFSIX-1-Cu (54-70) sets new benchmarks for SO<sub>2</sub>/CO<sub>2</sub> separation. The separation selectivities of SO<sub>2</sub>/N<sub>2</sub> and SO<sub>2</sub>/CH<sub>4</sub> on the SIFSIX materials were as well estimated by IAST. Figure 1 F shows the high SO<sub>2</sub>/N<sub>2</sub> selectivities on SIFSIX-1-Cu (2510-3145) and SIFSIX-2-Cu-i (1285-3103) over a wide range of  $SO_2$  molar fraction in gas phase (0.1–0.9). Moreover, high SO<sub>2</sub>/CH<sub>4</sub> selectivities (Figure S5, Supporting Information) over the same range of SO<sub>2</sub> molar fraction were also achieved on SIFSIX-1-Cu (992-1241), SIFSIX-2-Cu-i (422-1017), and SIFSIX-3-Ni (86-371). Therefore, SIFSIX-1-Cu and SIFSIX-2-Cu-i fulfill the requirements by FGD technology, natural-gas purification and other SO2-separation processes for both SO<sub>2</sub> capacity and selectivity.

To unravel the nature of the interactions between SO<sub>2</sub> molecule and SIFSIX materials, we performed modeling studies using first-principles DFT-D (dispersion-corrected density functional theory) calculations. When trapped within the pore of SIFSIX-1-Cu, SO2 gets adsorbed primarily through the  $S^{\delta_1} \cdots F^{\delta_-}$  electrostatic interaction (Figure 2) with SiF<sub>6</sub><sup>-</sup> anion and the multiple  $O^{\delta} \cdots H^{\delta+}$  dipole–dipole interactions with the 4,4'-bipyridine linker (Figure 2B). The DFT-D calculated S···F distance is  $\approx$ 2.6 Å (Figure 2A), much smaller than the sum of the van der Waals radii of S and F (3.3 Å), indicating the considerable strength of this interaction that arises from the negative nature of  $SiF_6^{2-}$  ion and positive charge of S atom. Simultaneously, the two oxygen atoms of SO<sub>2</sub> molecule are bonded by the 4,4'-bipyridine linker through multiple dipoledipole interactions, especially the  $O^{\delta-\cdots}H^{\delta+}$  interactions between oxygen atoms and aromatic hydrogens with a distance of 2.39-3.30 Å (Figure 2B). These multiple synergistic interactions enable the specific recognition of  $SO_2$  molecules through grasping every atoms of the adsorbed SO<sub>2</sub>, with a calculated strong adsorption energy ( $\Delta E$ ) of 50.3 kJ mol<sup>-1</sup>. Thanks to the four equivalent F sites and four equivalent aromatic linkers, four SO2 molecules were trapped firmly by the host-guest  $S^{\delta_{+}}\cdots F^{\delta}$  and  $O^{\delta_{-}}\cdots H^{\delta_{+}}$  interactions per unit cell. After that, it is noticed that there are still occupiable pore space in the unit cell of SIFSIX-1-Cu (between the F sites, along crystallography *c* direction) to accommodate more SO<sub>2</sub> guests. DFT-D calculations showed that two more SO<sub>2</sub> molecules could be trapped in this space as the secondary adsorption, through the dipole–dipole interactions with the channel pore surface and the intermolecular interaction (mainly dipole–dipole interaction) with the SO<sub>2</sub> adsorbed at the primary sites. The  $\Delta E$  of SO<sub>2</sub> on this site was 38.7 kJ mol<sup>-1</sup>, with a calculated nearest S<sub>site2</sub>···O<sub>site1</sub> distance of 3.6 Å. As a result, six SO<sub>2</sub> were trapped within per unit cell of SIFSIX-1-Cu, four of which were primarily adsorbed via host–guest interactions and the other two were secondarily accommodated mainly via guest–guest interaction with the primary SO<sub>2</sub>.

Previous studies have shown that the intermolecular distance in SO<sub>2</sub> liquid tested from X-ray diffraction and neutron studies were centered at 3.5, 4.5, and 5.6 Å with different types of orientations.<sup>[44,45]</sup> As clearly shown in Figure 2A, the intermolecular distance of adsorbed SO<sub>2</sub>(I) and SO<sub>2</sub>(II) is 3.32, 3.56, and 4.07 Å, respectively, within the distance range of the liquid SO<sub>2</sub>. These abovementioned data visualize the dense packing of "SO<sub>2</sub> clusters" within the confined electrostatic nanospace of SIFSIX-1-Cu, in consequence of the synergistic host–guest and guest–guest interactions. It is worth noting that this dense packing of "SO<sub>2</sub> clusters" at ambient temperature and low pressure has rarely been reported in common porous adsorbents.

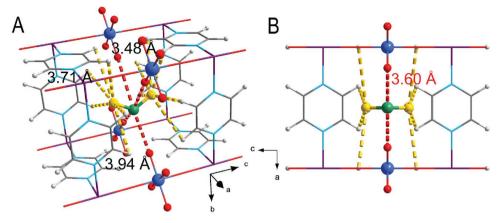
The dense packing of SO<sub>2</sub> clusters within SIFSIX materials is not only the result of the unique pore chemistry but also the optimal pore size. When the organic linker in SIFSIX-1-Cu was replaced by a longer analog, 4,4'-dipyridylacetylene, the resulted SIFSIX-2-Cu showed a weaker interaction with SO<sub>2</sub> (44.2 kJ mol<sup>-1</sup>) than SIFSIX-1-Cu. The S····F electrostatic interaction was basically of the same nature and strength in the two isoreticular MOFs, implied by the very similar S···F distances, but the dipole–dipole interaction between SO<sub>2</sub> and the 4,4'-dipyridylacetylene linker was slightly weaker than the 4,4'-bipyridine case because of the larger channel pore size of this SIFSIX material. The experimental SO<sub>2</sub> capacity of SIFSIX-2-Cu at room temperature and 1 bar was 6.5 mmol g<sup>-1</sup>, equivalent to ≈3.7 SO<sub>2</sub> per unit cell. This is lower than the capacity of SIFSIX-1-Cu that was 11.0 mmol g<sup>-1</sup> and equivalent to



**Figure 2.** A,B) DFT-D calculated SO<sub>2</sub> adsorption binding sites in SIFISX-1-Cu viewing in two different directions. Color code: F, red; Si, light blue; C, gray; H, light gray; N, sky blue; Cu, dark teal; O, orange; S, sea green (Note: the secondary adsorbed SO<sub>2</sub> molecules were highlighted with bright color).



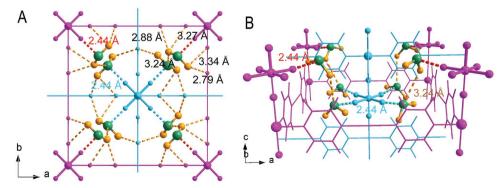




**Figure 3.** A,B) DFT-D calculated SO<sub>2</sub> adsorption binding sites in SIFISX-3-Zn viewing in two different directions. Color code: F, red; Si, light blue; C, gray; H, light gray; N, sky blue; Zn, violet; O, orange; S, sea green.

≈5.7 SO<sub>2</sub> per unit cell. A too small pore size also goes against the uptake of SO<sub>2</sub>. In SIFSIX-3-Zn, the channel pore size is small due to the much shorter linker pyrazine. DFT-D calculations show that SO<sub>2</sub> molecules get preferentially adsorbed at the center of the 1D channel of SIFSIX-3-Zn along the crystallography *c*-axis. Although the calculated  $\Delta E$  of SO<sub>2</sub> with SIFSIX-3-Zn was 54.1 kJ mol<sup>-1</sup>, slightly higher than that in SIFSIX-1-Cu, the much smaller pore volume captured less SO<sub>2</sub> than SIFSIX-1-Cu. The much longer S···F distance (3.60 Å) demonstrates a weaker S<sup> $\delta$ +···F<sup> $\delta$ </sup> interaction between SO<sub>2</sub> and SIFSIX-3-Zn (**Figure 3**) than the SIFSIX-1-Cu case, and the grasp of one SO<sub>2</sub> in SIFSIX-3-Zn consumes four times as much F sites as in SIFSIX-1-Cu.</sup>

The significance of a well-designed pore chemistry and pore size on the dense packing of SO<sub>2</sub> clusters was further highlighted by the modeling on SIFSIX-2-Cu-i. Although the organic linker in SIFSIX-2-Cu-i is the same as that in SIFSIX-2-Cu, the framework interpenetration in SIFSIX-2-Cu-i enables the size of its unit cell approximately half of that of SIFSIX-2-Cu with a more compact SiF<sub>6</sub><sup>2-</sup> distribution (**Figure 4**). DFT-D calculation showed that the S···F distance in this MOF is  $\approx 2.44$  Å, lower than those in other modeled SIFSIX materials, indicating a strong S<sup> $\delta_1$ </sup>···F<sup> $\delta$ </sup> electrostatic interaction between SO<sub>2</sub> and SiF<sub>6</sub><sup>2-</sup>. On the other hand, the two O atoms of SO<sub>2</sub> interact with the H atoms of 4,4'-dipyridylacetylene through multiple  $O^{\delta-}\cdots H^{\delta+}$  interactions, with  $O\cdots H$  distances of 2.79–3.34 Å (Figure 4A). In consequence, every atom of the adsorbed SO<sub>2</sub> was grasped by the pore surface of SIFSIX-2-Cu-i through these multiple synergistic host-guest interactions, with a  $\Delta E$ of  $\approx 50.2$  kJ mol<sup>-1</sup>. This is comparable to that in SIFSIX-1-Cu ( $\approx$ 50.3 kJ mol<sup>-1</sup>). The two SiF<sub>6</sub><sup>2-</sup> anions on the diagonal of each unit cell in SIFSIX-2-Cu-i enables the adsorption of two SO<sub>2</sub> by the host-guest  $S^{\delta_{+}} \cdots F^{\delta}$  and  $O^{\delta_{-}} \cdots H^{\delta_{+}}$  interactions. Interestingly, because those two SO2 molecules are located very close to each other, with the nearest  $S \cdots O$  distance of only  $\approx 3.2$  Å, which enhance the guest-guest interactions (Figure 4A,B). The cooperation of the host-guest and guest-guest interactions affords the formation of SO2 clusters within the confined electrostatic nanospace of SIFSIX-2-Cu-i. The nearest S····O distance of  $\approx$ 3.2 Å between two neighboring adsorbed SO<sub>2</sub> is comparable to the intermolecular distance (3.5-5.6 Å) in liquid crystal SO<sub>2</sub> phase and even slightly smaller than that in SIFSIX-1-Cu, implying a dense packing of SO<sub>2</sub> clusters within the pores of SIFSIX-2-Cu-i that enables the excellent uptake of SO<sub>2</sub> at low partial pressures. As presented in Table 1, the experimental SO<sub>2</sub> adsorption capacity of SIFSIX-2-Cu-i at room temperature and 0.01 bar was as large as 4.16 mmol g<sup>-1</sup>, much higher than those in SIFSIX-1-Cu (3.43 mmol g<sup>-1</sup>), SIFSIX-3-Zn and SIFSIX-3-Ni. Even if at 0.002 bar (2000 ppm) the SO<sub>2</sub> capacity was as high as 2.26 mmol g<sup>-1</sup>. Overall, DFT-D calculations on the different



**Figure 4.** A,B) DFT-D calculated  $SO_2$  adsorption sites in SIFISX-2-Cu-i viewing in two different directions, and C) crystal structure obtained from Rietveld refinement of PXRD data on  $SO_2$ -loaded SIFSIX-2-Cu-i. (Note: the different nets are highlighted in magenta and cyan for clarity).



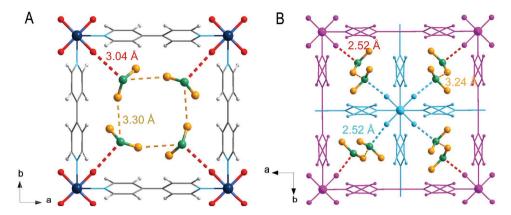


Figure 5. A,B) Crystal structure obtained from Rietveld refinement of PXRD data on SO<sub>2</sub>-loaded SIFSIX-1-Cu (A) and SIFSIX-2-Cu-i (B).

SIFSIX materials manifest that the excellent SO<sub>2</sub> capture performance of SIFSIX-1-Cu and SIFSIX-2-Cu-i can be attributed to the synergetic host–guest binding (electrostatic and dipole– dipole interactions) and cooperative guest–guest interactions within the confined electrostatic nanospace of moderate size to form SO<sub>2</sub> clusters.

To provide experimental proof for the DFT-D analysis of SO<sub>2</sub>-SIFSIX interactions, we have performed Rietveld refinement of the powder X-ray diffraction patterns of SO<sub>2</sub>-loaded samples to locate the adsorbed positions of SO<sub>2</sub> molecules in the crystal structure of SIFSIX materials, and the experimental results are well consistent with the DFT-D calculation results. The Rietveld refined data reveals that in the interpenetrated structure of SIFSIX-2-Cu-i, each SO<sub>2</sub> molecule indeed interacts with SIFSIX-2-Cu-i through S<sup> $\delta_{+}$ </sup>...F<sup> $\delta_{-}$ </sup> bonding (2.52 Å) and multiple O<sup> $\delta_{-}$ </sup>...H<sup> $\delta_{+}$ </sup> interactions (**Figure 5**B). The nearest S···O distance between adjacent SO<sub>2</sub> molecules are 3.2 Å. In SIFSIX-1-Cu, SO<sub>2</sub> also gets adsorbed primarily through the S<sup> $\delta_{+}$ </sup>...F<sup> $\delta_{-}$ </sup> electrostatic interaction with SiF<sub>6</sub><sup>-</sup> anion (Figure 5A). The S<sup> $\delta_{+}$ </sup>...F<sup> $\delta_{-}$ </sup> distance is 3.04 Å, longer than the modeling results (2.61 Å). Cooperative interactions between adjacent SO<sub>2</sub> molecules are also observed in the crystal structure of SIFSIX-1-Cu-SO<sub>2</sub> with a S···O distance of 3.3 Å.

We also have performed the detailed DFT-D calculations for CO<sub>2</sub>/N<sub>2</sub> molecules to illustrate the difference on interactions between SO<sub>2</sub> and N<sub>2</sub>/CO<sub>2</sub> molecules. Results show that the calculated  $C \cdots F$  distances between  $CO_2$  and  $SiF_6^{2-}$  (2.52) and 2.80 Å) in SIFSIX-2-Cu-i (Figure S10, Supporting Information) are longer than those between  $SO_2$  and  $SiF_6^{2-}$  binding sites (2.44 Å), indicating that SIFSIX-2-Cu-i interacted more strongly with SO2 than CO2. In SIFSIX-1-Cu, the calculated  $C \cdots F$  distance for  $CO_2$  (2.60 Å) is comparable to the  $S \cdots F$ distance for SO<sub>2</sub> (2.61 Å); however, the calculated  $O \cdots H$  distances between CO<sub>2</sub> molecule and 4,4'-bipyridine (2.64–3.58 Å) are longer than that of SO<sub>2</sub> system (2.39-3.30 Å) (Figure S11, Supporting Information). Additionally, the static adsorption energy ( $\Delta E$ ) results show that there are much stronger interactions with SO<sub>2</sub> than CO<sub>2</sub> ( $\Delta E$  in SIFSIX-2-Cu-i, 50.2 versus 35.7 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-1-Cu, 50.3 vs 31.1 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-3-Zn, 54.1 versus 45.7 kJ mol<sup>-1</sup>).

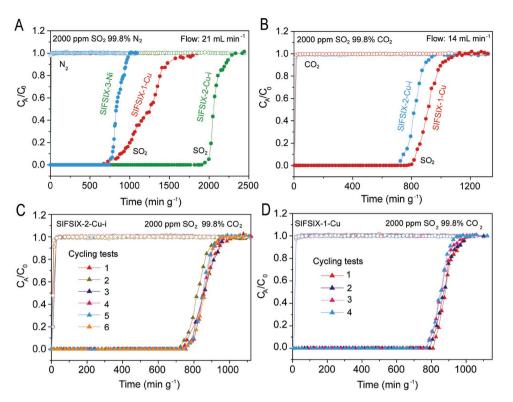
To confirm the actual  $SO_2/N_2$  and  $SO_2/CO_2$  separation performance on the SIFSIX materials, we conducted experimental breakthrough tests at 298 K and 1.01 bar on SIFSIX-2-Cu-i, SIFSIX-1-Cu, and SIFSIX-3-Ni (Figure 6).  $SO_2/N_2$  mixture

containing 2000 ppm SO<sub>2</sub> was used to mimic the flue gas with low concentration of SO2. The reason for using SIFSIX-3-Ni rather than SIFSIX-3-Zn is the relatively higher stability of SIFSIX-3-Ni (Figure S15, Supporting Information). As shown in Figure 6A, highly efficient elimination of SO2 was achieved with clean N<sub>2</sub> eluted from the bed by all the three SIFSIX materials. The breakthrough time of SO2 on SIFSIX-2-Cu-i (1800 min g<sup>-1</sup>) exceeded that on SIFSIX-1-Cu and SIFSIX-3-Ni, consistent with the higher SO<sub>2</sub> adsorption capacities of SIFSIX-2-Cu-i (2.31 mmol g<sup>-1</sup>) than SIFSIX-1-Cu (1.80 mmol g<sup>-1</sup>) and SIFSIX-3-Ni (1.39 mmol g<sup>-1</sup>) in static adsorption experiment at 298 K and 0.002 bar (Figure 1A). Additionally, the actual SO<sub>2</sub>/CO<sub>2</sub> separation performance on these SIFSIX materials was also confirmed by the breakthrough experiments, in which the SO<sub>2</sub>/CO<sub>2</sub> mixture containing 2000 ppm SO<sub>2</sub> was used. As shown in Figure 6B, outstanding efficient separation of SO2/CO2 was achieved with clean CO2 eluted from the bed by SIFSIX-1-Cu and SIFSIX-2-Cu-i, agreeing well with the results of adsorption isotherm and IAST calculations. The superb SO<sub>2</sub>/N<sub>2</sub> and SO<sub>2</sub>/CO<sub>2</sub> selectivity at very low SO<sub>2</sub> concentrations makes SIFSIX materials very promising for the gas desulfurization applications.

Given that SO<sub>2</sub> is highly corrosive and few porous MOF materials are stable to the presence of SO<sub>2</sub>, concerns about material regeneration are raised. Therefore, we conducted cycling breakthrough tests to evaluate the reusability of SIFSIX-2-Cu-i and SIFSIX-1-Cu for SO<sub>2</sub> capture. As the desorption curves shown in the Figure S16 (Supporting Information), SIFSIX materials adsorbed with SO<sub>2</sub> could be fully regenerated by He flow at 313 K. The breakthrough performance of SIFSIX-2-Cu-i and SIFSIX-1-Cu for 0.2/99.8 (SO<sub>2</sub>/CO<sub>2</sub>) mixture did not declined during 6 and 4 cycles, respectively (Figure 6C,D). And XRD patterns indicated that both of the SIFSIX materials retain their stability after breakthrough experiments (Figure S6, Supporting Information). In addition, moisture (1000 ppm) has slightly effect on the adsorption capacity of SO2 on SIFSIX-2-Cu-i (Figure S17, Supporting Information) and SIFSIX-2-Cu-i is stable when exposed to humidity (75%) (Figure S18, Supporting Information).

In summary, this work reports the selective recognition and dense packing of the so-called  $SO_2$  clusters in hybrid porous materials with inorganic-anion-pillared metal–organic framework for the first time. The multiple binding sites of anionic and aromatic linkers initiate the specific recognition of  $SO_2$  by host–guest interactions that grasp the every atom of  $SO_2$ 

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**Figure 6.** A,B) Experimental column breakthrough curves for  $SO_2/N_2$  (2000 ppm  $SO_2$ ) separations with SIFSIX-1-Cu, SIFSIX-2-Cu-i, and SIFSIX-3-Ni, and  $SO_2/CO_2$  (2000 ppm  $SO_2$ ) separations (A) and with SIFSIX-1-Cu and SIFSIX-2-Cu-i (B) at 298 K and 1.01 bar. C,D) Cycling column breakthrough tests for  $CO_2/SO_2$  (2000 ppm  $SO_2$ ) separations with SIFSIX-2-Cu-i (C) and SIFSIX-1-Cu (D) at 298 K and 1.01 bar (mixed gas flow: 14 mL min<sup>-1</sup>). In panel (A), open circles are for  $N_2$ , and filled circles are for  $SO_2$ . In panel (B), the open circles are for  $CO_2$ , and the filled circles are for  $SO_2$ .  $C_A/C_0$ , outlet concentration/feed concentration.

firmly, while the dipolar guest-guest interactions between SO2 molecules enforce the adsorption through promoting the primary binding and enabling secondary adsorption to form SO<sub>2</sub> clusters. A moderate pore size is crucial to afford adequate strength of synergistic host-guest and guest-guest interactions for a dense packing of SO<sub>2</sub>. Thanks to the suitable pore chemistry and size, SIFSIX-1-Cu showed exceptionally high adsorption capacity of SO<sub>2</sub> (11.01 mmol  $g^{-1}$  at 1.01 bar) and selectivity SIFSIX-2-Cu-i exhibited unprecedented SO<sub>2</sub> capacity at low pressures (4.16 mmol  $g^{-1}$  at 0.01 bar and 2.31 mmol  $g^{-1}$  at 0.002 bar) and record SO<sub>2</sub>/CO<sub>2</sub> selectivity (86-89), while SIFSIX-1-Cu showed exceptionally high adsorption capacity of SO<sub>2</sub> (11.01 mmol g<sup>-1</sup>) at 1.01 bar and also excellent SO<sub>2</sub>/CO<sub>2</sub> selectivity (54–70). Additionally, extraordinarily high SO<sub>2</sub>/N<sub>2</sub> selectivity was also achieved by SIFSIX-2-Cu-i (1285-3103) and SIFSIX-1-Cu (2510-3145). As further confirmed by the breakthrough experiments for mixed gases containing 2000 ppm SO<sub>2</sub>, this excellent performance sets a new benchmark in the highly efficient elimination of  $SO_2$  from flue gas or natural gas even if with a low SO2 concentration, and this work will be also instructive for the design of porous materials for other gas-purification processes.

#### **Experimental Section**

Materials: SIFSIX materials including SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were synthesized as

previously described in refs. [19] and [24] (see the Supporting Information for details).  $^{\left[ 19,24\right] }$ 

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 $SO_2$  Adsorption:  $SO_2$  adsorption isotherms at 298 and 273 K were collected using the apparatus in Figure S1 (Supporting Information). Activated samples were packed in a glass container which was partly immersed in a water bath. The  $SO_2$  adsorption isotherms were determined using  $SO_2/N_2$  mixed gas with varying  $SO_2$  molar fractions under flow mode. Note: the adsorption of  $SO_2$  at 1.01 bar was measured with pure  $SO_2$  at flow mode. At the beginning of this experiment, the activated sample was loaded in the glass container which was full of pure  $N_2$  atmosphere at 760 mmHg. Then, the  $SO_2/N_2$  mixed gas (e.g., 0.002/99.998) was introduced at a constant flow at 760 mmHg. Adsorption equilibrium was reached until the weight of glass container kept constant and did not change. The  $SO_2$  uptake was calculated based on the weight change before and after dynamic adsorption (see the Supporting Information for more detailed adsorption procedures).

Breakthrough Tests: The breakthrough experiments were carried out in a dynamic gas breakthrough equipment (see Figure S2 in the Supporting Information).<sup>[39]</sup> All experiments were conducted using a stainless steel column (4.6 mm inner diameter × 50 mm). According to the different particle size and density of the sample powder, the weight packed in the column was: SIFSIX-1-Cu powder (0.21 g), SIFSIX-2-Cu-i (0.21 g), and SIFSIX-3-Ni (0.50 g), respectively. The column packed with sample was first purged with He flow (15 mL min<sup>-1</sup>) for 12 h at room temperature (25 °C). The mixed gas of SO<sub>2</sub>/N<sub>2</sub> = 0.2/99.8 (v/v) was then introduced at 21 mL min<sup>-1</sup>, and SO<sub>2</sub>/CO<sub>2</sub> = 0.2/99.8 (v/v) was introduced at 14 mL min<sup>-1</sup>. Outlet gas from the column was monitored using gas chromatography (GC-2010 plus) with a thermal conductivity detector (TCD) coupled with a FID. The gas mixture was separated by a capillary column (Agilent GS-GASPRO,  $\Phi$ 0.32 × 60 m). The concentration of SO<sub>2</sub>, CO<sub>2</sub> or N<sub>2</sub> in the outlet gas was monitored by the TCD. After the





breakthrough experiment, the sample was regenerated with He flow (7 to 15 mL min^-1) for 6–20 h.

Density-Functional Theory Calculations: First-principles densityfunctional theory (DFT) calculations were performed using the Quantum-Espresso package. A semi-empirical addition of dispersive forces to conventional DFT was included in the calculation to account for van der Waals interactions.<sup>[46]</sup> Vanderbilt-type ultrasoft pseudopotentials and generalized gradient approximation with Perdew-Burke-Ernzerhof exchange correlation were used. A cutoff energy of 544 eV and a 2  $\times$  2  $\times$  4 k-point mesh (generated using the Monkhorst-Pack scheme) were found to be enough for the total energy to converge within 0.01 meV atom-1. The structure of SIFSIX MOFs was first optimized. The optimized structures are good matches for the experimentally determined crystal structures of the coordination networks. Various guest gas molecules were then introduced to various locations of the channel pore, followed by a full structural relaxation. To obtain the gas binding energy, an isolated gas molecule placed in a supercell (with the same cell dimensions as the MOF crystal) was also relaxed as a reference. The static binding energy (at T = 0 K) was then calculated using:  $E_{\rm B} = E({\rm MOF}) + E({\rm gas}) - E({\rm MOF} + {\rm gas}).$ 

Fitting of Isotherms: The isotherm data for SO<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> in SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were fitted with either the Langmuir–Freundlich isotherm model:

$$q = q_{\rm sat} \frac{bp^{\nu}}{1 + bp^{\nu}} \tag{1}$$

with *T*-dependent parameters *b*:

$$b = b_0 \exp\left(\frac{E}{RT}\right) \tag{2}$$

IAST Calculations of Adsorption Selectivities: The adsorption selectivity for  $C_2H_2/C_2H_4$  separation is defined by:

$$S_{ads} = \frac{q_1/q_2}{p_1/p_2}$$
(3)

where  $q_1$  and  $q_2$  are the molar loadings in the adsorbed phase in equilibrium with the bulk gas phase with partial pressures  $p_1$ , and  $p_2$ .

#### **Supporting Information**

Supporting Information is available from the Wiley Online Library or from the author.

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#### **Conflict of Interest**

The authors declare no conflict of interest.

#### **Keywords**

adsorption, gas purification, ionic hybrid porous materials,  $\mathsf{SO}_2$  cluster, sulfur dioxide

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## ADVANCED MATERIALS

## **Supporting Information**

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Ultrahigh and Selective SO<sub>2</sub> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials

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## Supporting Information

#### Ultrahigh and Selective SO<sub>2</sub> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials

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#### This PDF file includes:

Materials and Methods

Tables S1-S6

Figures. S3 to S18

#### **Experiments**

#### Materials

Ammonium hexafluorosilicate ((NH)<sub>2</sub>SiF<sub>6</sub>, 98%, Aldrich), copper (II) tetrafluoroborate hydrate (Cu(BF<sub>4</sub>)<sub>2</sub>• xH<sub>2</sub>O, 98%, Aldrich), zinc hexafluorosilicate hydate (ZnSiF<sub>6</sub>• xH<sub>2</sub>O, 99%, Aldrich), 4,4'-bipyridine (C<sub>10</sub>H<sub>8</sub>N<sub>2</sub>, 98%, Aldrich), 4-(2-pyridin-4-ylethynyl)pyridine (C<sub>12</sub>H<sub>8</sub>N<sub>2</sub>, 98%, Chemsoon), pyrazine (C<sub>4</sub>H<sub>4</sub>N<sub>2</sub>, 99%, Aldrich), methanol (CH<sub>3</sub>OH, anhydrous, 99%, Sigma-Aldrich), ethylene glycol (C<sub>2</sub>H<sub>6</sub>O<sub>2</sub>, anhydrous, 99%, Sigma-Aldrich), were purchased and used without further purification.

N<sub>2</sub> (99.999%), CO<sub>2</sub> (99%), CH<sub>4</sub> (99.99%), He (99.999%), SO<sub>2</sub> (99.99%) and mixed gases of (1) SO<sub>2</sub>/N<sub>2</sub> = 0.2/99.8 (v/v), (2) SO<sub>2</sub>/N<sub>2</sub> = 1/99 (v/v), (3) SO<sub>2</sub>/N<sub>2</sub> = 5/95 (v/v), (4) SO<sub>2</sub>/N<sub>2</sub> = 10/90 (v/v) were purchased form JinGong Company (China). Mixed gases of (5) SO<sub>2</sub>/CO<sub>2</sub> = 0.2/99.8 (v/v) were purchased from Shanghai Wetry Standard Reference Gas Analytical Technology Co. LTD (China).

#### **Synthesis**

Synthesis of SIFSIX-1-Cu (Cu(4,4'-bipyridine)<sub>2</sub>SiF<sub>6</sub>•8H<sub>2</sub>O)n

Firstly, 4,4'-bipyridine (0.35 g) was dissolved in ethylene glycol (40 mL) at 338 K. An aqueous solution (20 mL) of  $Cu(BF_4)_2 \cdot xH_2O$  (266 mg, 1.12 mmol) and  $(NH_4)_2SiF_6$  (199 mg, 1.12 mmol) was added to the above solution. Then the mixture was heated at 65 °C for 3 h under stirring. The obtained purple powder was filtered, washed with methanol, and was exchanged with methanol for 3 days.<sup>[1]</sup>

Synthesis of SIFSIX-2-Cu (Cu(4,4'-bipyridylacetylene)<sub>2</sub>SiF<sub>6</sub>)n

An ethanol solution (2.0 mL) of 4,4'-bipyridylacetylene (0.115mmol) was carefully layered onto an ethylene glycol solution (2.0 mL) of  $CuSiF_6 \cdot xH_2O$  (0.149 mmol). Crystals of SIFSIX-2-Cu were obtained after two weeks. The obtained sample was exchanged with ethanol for 4 days.<sup>[2]</sup>

Synthesis of SIFSIX-2-Cu-i (Cu(4,4'-bipyridylacetylene)<sub>2</sub>SiF<sub>6</sub>).

A methanol solution (4.0 mL) of 4,4'-bipyridylacetylene (0.286 mmol) was mixed with an aqueous solution (4.0 mL) of  $Cu(BF_4)_2 \cdot xH_2O$  (0.26 mmol) and  $(NH_4)_2SiF_6$  (0.26 mmol) and then heated at 85 °C for 12 h. The obtained sample was exchanged with methanol for 3 days. [2]

#### Synthesis of SIFSIX-3-Zn (Zn(pyrazine)<sub>2</sub>SiF<sub>6</sub>)n

A methanol solution (2.0 mL) of pyrazine (1.3mmol) was carefully layered onto a methanol solution (2.0 mL) of ZnSiF<sub>6</sub>• xH<sub>2</sub>O (0.13 mmol). Colourless crystals of SIFSIX-3-Zn were obtained after two days. The obtained sample was exchanged with ethanol for 1 days. <sup>[2]</sup> Synthesis of SIFSIX-3-Ni (Ni(pyrazine)<sub>2</sub>SiF<sub>6</sub>)n

A methanol solution (20 ml) of nickel silicofluoride,  $NiSiF_6$  (1mmol) and pyrazine (2mmol) was mixed and heated at 85 °C. Blue powder was obtioned after 3days. The obtained sample was exchanged with ethanol for 3 days.<sup>[3]</sup>

#### Pure gas adsorption

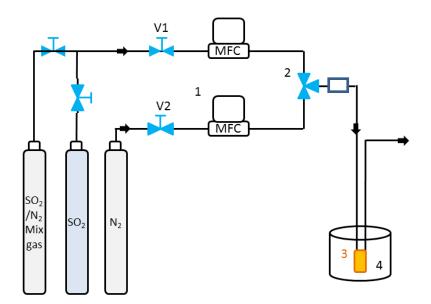
SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, and SIFSIX-3-Zn were evacuated at 303 K for 1-2 days until the pressure dropped below 7µm Hg. SIFSIX-3-Ni was degased at 105 °C for 15 h under dynamic pressure below 5µm Hg. N<sub>2</sub>, CO<sub>2</sub> and CH<sub>4</sub> sorption isotherms were collected at 298 K on activated SIFSIX-1-Cu, SIFSIX-2-Cu, SIDSIX-2-Cu-i, SIFSIX-3-Ni and SIFSIX-3-Zn using ASAP 2050 Analyzer (Micromeritics).

#### SO<sub>2</sub> adsorption

 $SO_2$  adsorption isotherms at 298 K and 273 K were collected using the apparatus in Figure S1. Activated samples were packed in a glass container which was partly immersed in a water bath. The  $SO_2$  adsorption isotherms were determined using  $SO_2/N_2$  mixed gas with varying  $SO_2$  molar fractions under flow mode. Note: the adsorption of  $SO_2$  at 1.0 atm was measured with pure  $SO_2$  at flow mode. At the beginning of this experiment, the activated sample was loaded in the glass container which was full of pure  $N_2$  atmosphere at 760 mmHg. Then the  $SO_2/N_2$  mixed gas (e.g. 0.002/99.998) was introduced at a constant flow at 760 mmHg.

Adsorption equilibrium was reached until the weight of glass container kept constant and didn't change. The SO<sub>2</sub> uptake was calculated based on the weight-change before and after dynamic adsorption. This method will underestimate the SO<sub>2</sub> uptake because the samples were pre-saturated by  $N_2$  but some of  $N_2$  molecules were displaced by the SO<sub>2</sub> molecules. At the adsorption with high SO<sub>2</sub> molar fraction, the weight of unabsorbed SO<sub>2</sub> gases in the glass container was subtracted by blank test.

The detailed adsorption procedures: firstly, SO<sub>2</sub>/N<sub>2</sub> (0.002/0.998) mixed gas was introduced into the glass container at a rate of 20 ml min<sup>-1</sup>. Equilibrium were reached until the weight of glass container kept constant and didn't change. The amount of adsorbed SO<sub>2</sub> at the partial pressure of 0.002 was determined by the electronic balance with  $\pm$  0.1 mg accuracy. Then, the uptake capacity of SO<sub>2</sub> at the partial pressure of 0.01, 0.05, 0.1 was measured using SO<sub>2</sub>/N<sub>2</sub> (0.01/0.99), SO<sub>2</sub>/N<sub>2</sub> (0.05/0.95), SO<sub>2</sub>/N<sub>2</sub> (0.1/0.9) mixed gas using the repeated procedures. The higher partial pressure of SO<sub>2</sub> (e.g. 0.4, 0.5, 0.8 1.0) was controlled by changing the flow rate of SO<sub>2</sub> and N<sub>2</sub>.



Mass flow controller 2. 3-Way valve 3. Glass container 4. Water bath
 Figure S1 Schematic illustration of the apparatus for the SO<sub>2</sub> adsorption experiments.

#### Breakthrough tests

The breakthrough experiments were carried out in a dynamic gas breakthrough equipment (fig. S2). <sup>[4]</sup> All experiments were conducted using a stainless steel column (4.6 mm inner diameter × 50 mm). According to the different particle size and density of the sample powder, the weight packed in the column was: SIFSIX-1-Cu powder (0.21 g), SIFSIX-2-Cu-i (0.21 g), and SIFSIX-3-Ni (0.50 g), respectively. The column packed with sample was firstly purged with He flow (15 ml min<sup>-1</sup>) for 12 h at room temperature (25 °C). The mixed gas of SO<sub>2</sub>/N<sub>2</sub> = 0.2/99.8 (v/v) was then introduced at 21 ml min<sup>-1</sup>, and SO<sub>2</sub>/CO<sub>2</sub> = 0.2/99.8 (v/v) ) was introduced at 14 ml min<sup>-1</sup>. Outlet gas from the column was monitored using gas chromatography (GC-2010 plus) with a thermal conductivity detector (TCD) coupled with a FID. The gas mixture was separated by a capillary column (Agilent GS-GASPRO,  $\Phi 0.32 \times 60 \text{ M}$ ). The concentration of SO<sub>2</sub>, CO<sub>2</sub> or N<sub>2</sub> in the outlet gas was monitored by the TCD. After the breakthrough experiment, the sample was regenerated with He flow (7 to 15 ml min<sup>-1</sup>) for 6 to 20 hours.

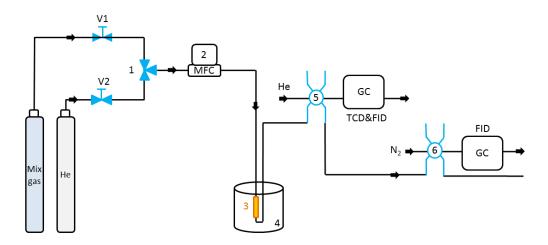


Figure S2 Schematic illustration of the apparatus for the breakthrough experiments.

#### X-ray diffraction structure analysis

Powder X-ray diffraction patterns were collected using SHIMADZU XRD-6000 diffractometer (Cu K<sub> $\alpha$ </sub>  $\lambda$  = 1.540598 Å) with an operating power of 40 Kv and fixed divergence slit of 0.76 mm. The data were collected in the range of 2 $\theta$  = 3-50°.

Powder X-ray diffraction patterns of bare and SO<sub>2</sub>-loaded SIFSIX-1-Cu and SIFSIX-2-Cu-i were collected using PANalytical X'Pert Pro diffractometer (Cu K<sub> $\alpha$ </sub>  $\lambda$  = 1.540598 Å) with an operating power of 40 Kv and fixed divergence slit of 0.380 mm. The data were collected in the range of 2 $\theta$  = 3-60°.

#### **Density-functional theory calculations**

First-principles density-functional theory (DFT) calculations were performed using the Quantum-Espresso package. A semi-empirical addition of dispersive forces to conventional DFT was included in the calculation to account for van der Waals interactions.<sup>[5]</sup> We used Vanderbilt-type ultrasoft pseudopotentials and generalized gradient approximation (GGA) with Perdew-Burke-Ernzerhof (PBE) exchange correlation. A cutoff energy of 544 Ev and a  $2\times 2\times 4$  k-point mesh (generated using the Monkhosrt-Pack scheme) were found to be enough for the total energy to converge within 0.01 meV atom<sup>-1</sup>. We first optimized the structure of SIFSIX MOFs. The optimized structures are good matches for the experimentally determined crystal structures of the coordination networks. Various guest gas molecules were then introduced to to various locations of the channel pore, followed by a full structural relaxation. To obtain the gas binding energy, an isolated gas molecule placed in a supercell (with the same cell dimensions as the MOF crystal) was also relaxed as a reference. The static binding energy (at T = 0 K) was then calculated using: EB = E(MOF) + E(gas) – E(MOF+gas).

#### Fitting of isotherms

The isotherm data for SO<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> in SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were fitted with either the Langmuir-Freundlich isotherm model.

$$q = q_{sat} \frac{bp^{\nu}}{1 + bp^{\nu}} \tag{1}$$

with T-dependent parameters b

$$b = b_0 \exp\left(\frac{E}{RT}\right) \tag{2}$$

The fitted parameter values are presented in Table S1

Notation

b	Langmuir-Freundlich constant, $Pa^{-\nu}$
Ε	energy parameter, J mol <sup>-1</sup>
р	pressure, Pa
q	component molar loading, mol kg <sup>-1</sup>
$q_{ m sat}$	saturation loading, mol kg <sup>-1</sup>
R	gas constant, 8.314 J mol <sup>-1</sup> K <sup>-1</sup>
Т	absolute temperature, K

#### Isosteric heat of adsorption

The binding energy of SO<sub>2</sub> is reflected in the isosteric heat of adsorption,  $Q_{\rm st}$ , defined as

$$Q_{st} = RT^2 \left(\frac{\partial \ln p}{\partial T}\right)_q \tag{3}$$

Figure S3 presents a comparison of the heats of adsorption of  $SO_2$  in various SIFSIX; the calculations are based on the use of the Clausius-Clapeyron equation.

#### IAST claculations of adsorption selectivities

The adsorption selectivity for C<sub>2</sub>H<sub>2</sub>/C<sub>2</sub>H<sub>4</sub> separation is defined by

$$S_{ads} = \frac{q_1/q_2}{p_1/p_2}$$
(3)

 $q_1$ , and  $q_2$  are the molar loadings in the adsorbed phase in equilibrium with the bulk gas phase with partial pressures  $p_1$ , and  $p_2$ .

**Table S1.** Langmuir-Freundlich parameter fits for SO<sub>2</sub>, CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> in SIFSIX materials. The isotherm data for CH<sub>4</sub>, and N<sub>2</sub> were only measured at 298 K, and therefore E = 0.

		SIFSIX-1-Cu	1	
	$q_{\rm sat}$	$b_0$	E	$\mathcal{V}$
	mol kg <sup>-1</sup>	$\mathrm{Pa}^{-\nu_i}$	kJ mol <sup>-1</sup>	dimensionless
$SO_2$	11.7	9.8×10 <sup>-8</sup>	26	0.72
$CO_2$	12	1.12×10 <sup>-13</sup>	33	1.2
CH <sub>4</sub>	12	3.9×10 <sup>-7</sup>	0	1
$N_2$	12	1.54×10 <sup>-7</sup>	0	1

		SIFSIX-2-Cu-	-i	
	$q_{\rm sat}$	$b_0$	E	ν
	mol kg <sup>-1</sup>	$\mathrm{Pa}^{-\nu_i}$	kJ mol <sup>-1</sup>	dimensionless
$SO_2$	7.1	1.33×10 <sup>-6</sup>	23.6	0.62
$CO_2$	6.5	4.9×10 <sup>-11</sup>	33	1
$CH_4$	12	4.87×10 <sup>-7</sup>	0	1
$N_2$	12	1.6×10 <sup>-7</sup>	0	1

SIFSIX-3-Ni Ε v  $b_0$  $q_{
m sat} \ {
m mol} \ {
m kg}^{-1}$ kJ mol<sup>-1</sup>  $Pa^{-\nu_i}$ dimensionless  $SO_2$ 2.7 3.05×10<sup>-11</sup> 46.2 1.07  $\mathrm{CH}_4$ 12  $3.9 \times 10^{-7}$ 0 1 12 0 1  $2.08 \times 10^{-7}$  $N_2$ 

		SIFSIX-3-Zn	l	
	$q_{\rm sat}$ mol kg <sup>-1</sup>	$b_0$		V
	mol kg <sup>-1</sup>	$Pa^{-\nu_i}$	kJ mol <sup>-1</sup>	dimensionless
$SO_2$	2.25	4.1×10 <sup>-6</sup>	23.5	0.52
CH <sub>4</sub>	12	3.78×10 <sup>-7</sup>	0	1
$N_2$	12	2.08×10 <sup>-7</sup>	0	1

**Table S2.** The volumetric uptake of  $SO_2$  (density per crystal cell volume) in various SIFSIX materials at 1.01 bar.

	Framawark danaity	$C_2H_2$ density per crystal cell volume (g cm <sup>-3</sup> )		
	Framework density (g cm <sup>-3</sup> )	298 K	283 K	
	(g chi )		273 K	
SIFSIX-1-Cu	0.864	0.609	0.658	
SIFSIX-2-Cu-i	1.247	0.551	0.575	
SIFSIX-3-Zn	1.574	0.212	0.237	
SIFSIX-3-Ni	1.610	0.282	0.299	

Atom	а	b	С
N6	0.00000	0.18296	0.00000
C5	0.00000	0.43393	0.00000
C1	0.03427	0.24303	0.13464
C2	0.03491	0.36849	0.13817
Н3	0.06405	0.19281	0.24102
H4	0.06545	0.41511	0.24710
Cu7	0.00000	0.00000	0.00000
Si8	0.00000	0.00000	0.50000
F9	0.00000	0.00000	0.28490
F10	0.10630	0.10630	0.50000
S11	0.28855	0.30438	0.56560
O12	0.40425	0.26932	0.49696
O13	0.21666	0.39012	0.47061

Table S3.	List	ofa	tomic	positions	for	SIFSIX-1-Cu $\cdot$ SO <sub>2</sub>

	Unit cell parameters
Formula sum	N C3 H2 Cu Si F2 S0.252 O0.503
Formula weight	197.81 g mol <sup>-1</sup>
Space-group	P 422
Cell	a=11.1348 Å b=11.1348 Å c=8.0047 Å α=90.00°
parameters	β=90.00° γ=90.00°
Cell ratio	a/b=1.0000 b/c=1.3910 c/a=0.7189
Cell volume	992.47 Å <sup>3</sup>

				1
2 Theta	h	k	1	d-
7.934	1	0	0	spacing 11.1348
11.044	0	0	0	8.00474
11.044	1	0 1	0	7.87352
13.613	1	1 0	1	6.49954
15.775	1	0	1	5.61324
15.775	2	$1 \\ 0$	1 0	5.56742
13.900	2	0	0	4.97965
17.798		1 0	0	4.97903 4.57062
20.993	2 2	0	1	4.37062 4.22826
		$1 \\ 0$	1 2	
22.193				4.00237
22.568	2	2	0	3.93676
22.602	1	0	2	3.76645
23.956	3	0	0	3.71162
24.937	1	1	2	3.56786
25.189	2	2	1	3.53265
25.273	3	1	0	3.52115
26.448	3	0	1	3.36725
27.423	2 3	0	2	3.24977
27.654		1	1	3.2231
28.591	2	1	2	3.11962
28.887	3	2	0	3.08825
31.013	3	2	1	2.88126
31.859	2	2	2	2.80662
32.129	4	0	0	2.78371
32.884	3	0	2	2.7215
33.146	4	1	0	2.7006
33.559	0	0	3	2.66825
33.880	3	1	2	2.64368
34.072	4	0	1	2.62926
34.136	3	3	0	2.62451
34.539	1	0	3	2.59479
35.039	4	1	1	2.55889
35.494	1	1	3	2.52708
35.983	3	3	1	2.49389
36.044	4	2	0	2.48983
36.728	3	2	2	2.44501
37.342	2	0	3	2.40618
37.810	4	2	1	2.37747
38.237	2	1	3	2.35189
39.396	4	0	2	2.28531
40.253	4	1	2	2.23865
40.473	5	0		2.22697
40.473	4	3	0	2.22697
40.822	2	2	3	2.20873
41.094	$\frac{2}{3}$	2 3	2	2.19473
41.311	5	1	$\overset{2}{0}$	2.19473
41.654	3	1 0	3	2.16651
71.007	5	12	5	2.10031

Table S4. List of Miller Index of the simulated pattern of SIFSIX-1-Cu+SO $_2$ 

42.082	5	0	1	2.14549
42.082	4	3	1	2.14549
42.473	3	1	3	2.12663
42.736	4	2	2	2.11413
42.894	5	1	1	2.10674
43.745	5	2	0	2.06769
44.856	3	2	3	2.01903
42.259	5	2	1	2.00198
45.278	0	0	4	2.00119
46.045	1	0	4	1.96963
46.075	4	4	0	1.96838
46.636	4	3	2	1.94601
46.636	5	0	2	1.94601
46.802	1	1	4	1.93952
47.143	4	0	3	1.92626
47.386	5	1	2	1.91696
47.531	4	4	1	1.91144
47.579	5	3	0	1.90961
47.887	4	1	3	1.89807
48.288	2	0	4	1.88322
48.622	3	3	3	1.87108
49.001	5	3	1	1.85749
49.019	2	1	4	1.85685
49.048	6	0	0	1.85581
49.583	5	2	2	1.83703
49.770	6	1	0	1.83056
50.068	4	2	3	1.82038
50.439	6	0	1	1.80786
51.146	6	1	1	1.78449
51.164	2	2	4	1.78393
51.711	4	4	2	1.76633
51.864	3	0	4	1.76147
51.893	6	2	0	1.76057
52.558	3	1	4	1.73983
52.586	3 5	4	0	1.73897
53.095	5	3	2	1.72349
53.229	6	2	1	1.71948
53.557	4	3	3	1.70972
53.557	5	0	3 3	1.70972
53.911	5	4	1	1.69933
54.236	5	1	3	1.68992
54.455	6	0	2	1.68363
54.603	3	2	4	1.67941

		1	
Atom	а	b	С
N7	0.00000	0.14897	0.00000
C5	0.00000	0.64726	0.00000
C1	0.02267	0.19911	0.13599
C2	0.02503	0.30009	0.14229
H3	0.03526	0.15749	0.24709
H4	0.03655	0.33606	0.25900
C6	0.00000	0.54419	0.00000
Cu8	0.00000	0.00000	0.00000
Si9	0.00000	0.00000	0.50000
F10	0.00000	0.00000	0.28300
F11	0.08780	0.08780	0.50000
<b>S</b> 7	0.19765	0.22777	0.57535
O5	0.26019	0.19711	0.44227
O6	0.12431	0.30126	0.53996

Table S5.	List	of atomic	positions	for	SIFSIX-2-Cu-i•SO <sub>2</sub>	

Unit cell parameters			
Formula sum	N C3 H Cu Si F2 S0.17 O0.341		
Formula weight	191.591 g mol <sup>-1</sup>		
Space-group	I 4/ m m m		
Cell parameters	a=13.7315 Å c=8.2100 Å		
Cell ratio	a/b=1.0000 b/c=1.6725 c/a=0.5979		
Cell volume	1548.04 Å <sup>3</sup>		

2 Theta	h	k	1	d-spacing
9.101	1	1	0	9.70963
12.552	1	0	1	7.04657
12.884	2	0	0	6.86575
18.024	2	1	1	4.9175
18.259	2	2	0	4.85482
20.436	3	1	0	4.34228
21.631	0	0	2	4.10502
22.218	3	0	1	3.99784
23.510	1	1	2	3.78099
25.257	2	0	2	3.52329
25.766	3	2	1	3.45482
25.934	4	0	0	3.43287
27.537	3	3	0	3.23654
28.451	2	2	2	3.13464
28.908	4	1	1	3.08613
29.059	4	2	0	3.07046
29.930	3	1	2	2.98304
33.242	5	1	$\frac{1}{0}$	2.69297
33.358	1	0	3	2.6839
34.017	4	0	2	2.63341
34.407	4	3	1	2.60445
34.407	5	0	1	2.60445
35.285	3	3	2	2.54159
35.897	2	1	3	2.49969
36.515	4	2	2	2.45875
36.882	5	2	1	2.43513
37.004	3 4	4	1 0	2.43313
38.186	5	4	0	2.42741 2.35493
	3	0	03	
38.288				2.34886
39.338	6	0	0	2.28858
40.010	5	1	2	2.25169
40.560	3	2	3	2.2224
41.451	6	1	1	2.17666
41.561	6	2	0	2.17114
42.731	4	1	3	2.11439
43.266	4	4	2	2.08944
43.585	5	4	1	2.07488
44.085	0	0	4	2.05251
44.309	5	3	2	2.04268
45.112	1	1	4	2.00813
45.332	6	0	2	1.99892
45.639	6	3	1	1.98617
46122	2	0	4	1.96652
46.740	7	1	0	1.94193
46.740	5	5	0	1.94193
46.827	4	3	3	1.93852
46.827	5	0	3	1.93852

**Table S6.** List of Miller Index of the simulated pattern of SIFSIX-2-Cu-i•SO $_2$ 

47.326	6	2	2	1.91923
47.624	7	0	1	1.90794
47.723	6	4	0	1.90422
48.091	2	2	4	1.8905
48.774	5	2	3	1.86558
49.053	3	1	4	1.85565
49.547	7	2	1	1.83828
50.583	7	3	0	1.80303
51.859	4	0	4	1.76164
52.056	7	1	2	1.75542
52.056	5	5	2	1.75542
52.506	6	1	3	1.74143
52.770	3	3	4	1.73335
52.965	6	4	2	1.72741
53.240	6	5	1	1.71916
53.331	8	0	0	1.71644
53.670	4	2	4	1.70637
54.303	5	4	3	1.68798

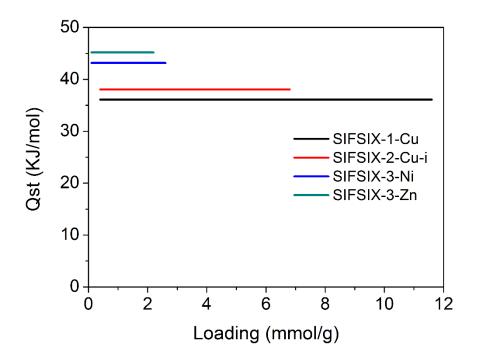


Figure S3 Comparison of  $Q_{st}$  of SO<sub>2</sub> adsorption in SIFSIX materials.

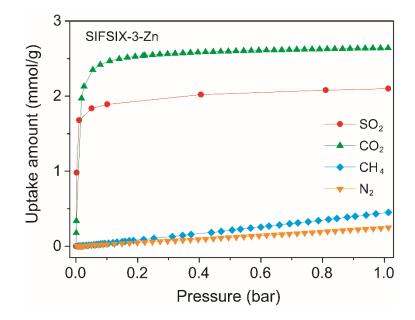


Figure S4 Adsorption isotherms for  $SO_2$ ,  $CO_2$  and  $CH_4$  on SIFSIX-3-Zn at 298 K and 1.0 bar. Note: the adsorption isotherm of  $SO_2$  were determined using  $SO_2/N_2$  mixed gas with varying  $SO_2$  molar fractions under flow mode.

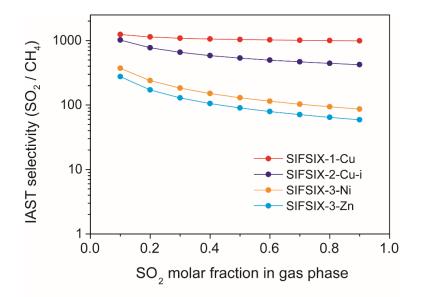
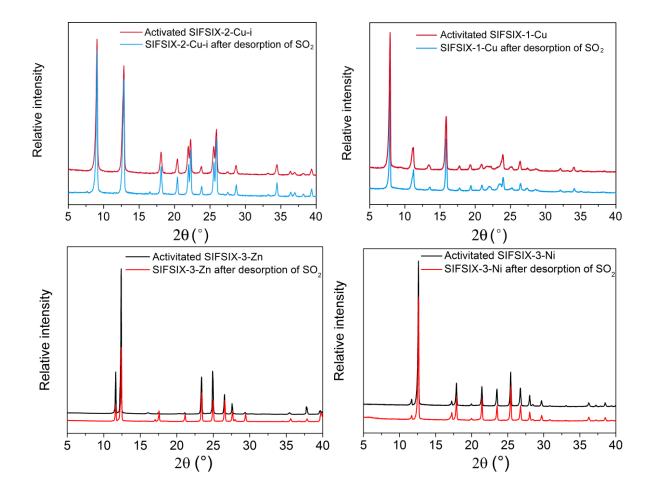


Figure S5 IAST selectivities of  $SO_2/CH_4$  on SIFSIX materials with varying  $SO_2$  molar fractions in gas phase at 100 kPa.



**Figure S6.** PXRD patterns of sample SIFSIX-2-Cu-i (A), SIFSIX-1-Cu (B), SIFSIX-3-Zn (C) and SIFSIX-3-Ni (D).

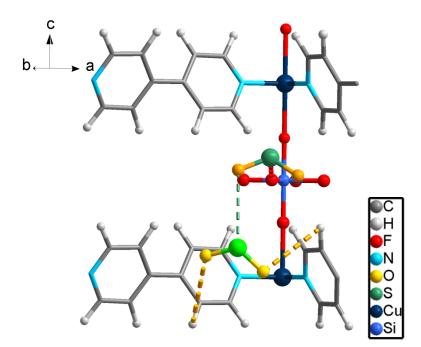
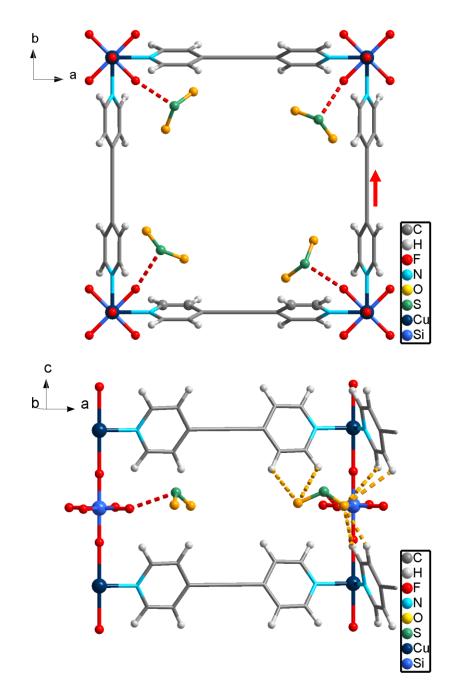
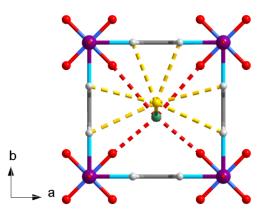


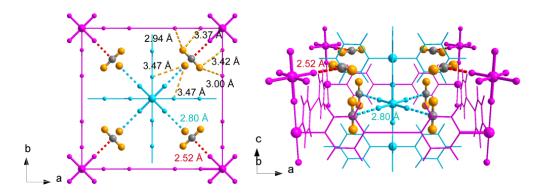
Figure S7 Schematic pictures from DFT-D simulation reveal the  $SO_2$  adsorbed at the secondary adsorption sites of SIFSIX-1-Cu through diploe-diploe interactions. (Note: the secondary adsorbed  $SO_2$  molecules were highlighted with bright colour).



**Figure S8** DFT-D simulated optimized SO<sub>2</sub> adsorption sites of SIFSIX-2-Cu in two different viewing directions (A and B).

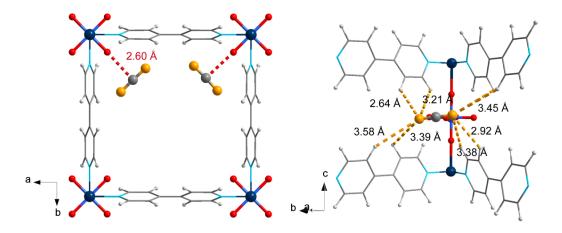


**Figure S9** DFT-D simulated optimized SO<sub>2</sub> adsorption sites of SIFSIX-3-Zn viewed down the c axis.



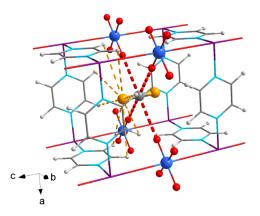
**Figure S10**. DFT-D calculated  $CO_2$  adsorption sites in SIFISX-2-Cu-i viewing in two different directions (A and B). (Note: the different nets are highlighted in magenta and cyan for clarity).

As shown in Figure S10, CO<sub>2</sub> were trapped in the interpenetrated SIFSIX-2-Cu-i through  $C^{\delta^+} \cdots F^{\delta^-}$  and multiple  $O^{\delta^-} \cdots H^{\delta^+}$  interactions. The DFT-D calculated distance of C $\cdots$ F from different nets are 2.80 and 2.52 Å, respectively (Figure S10). By contrast, the DFT-D calculated distance of S $\cdots$ F from different nets are both 2.44 Å, indicating much stronger electrostaic interactions between SO<sub>2</sub> and SIFSIX-2-Cu-i.



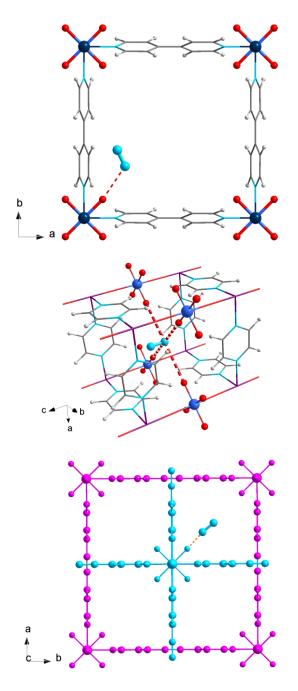
**Figure S11**. DFT-D calculated CO<sub>2</sub> binding sites in SIFSIX-1-Cu viewing in two different directions (A and B). Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Cu, dark teal; O, orange.

In SIFSIX-1-Cu, the adsorbed CO<sub>2</sub> are bound by the  $C^{\delta^+} \cdots F^{\delta^-}$  (Figure S11A) and multiple  $O^{\delta^-} \cdots H^{\delta^+}$  (Figure S11B) interactions. The DFT-D calculated distance of C $\cdots$ F (2.60 Å) is comparable to the calculated distance of S $\cdots$ F is 2.61 Å. And the DFT-D calculated O $\cdots$ H distance of CO<sub>2</sub> molecule with 4,4'-bipyridine ranged form 2.64 ~ 3.58 Å, longer than the O $\cdots$ H distance of SO<sub>2</sub> molecule with 4,4'-bipyridine (2.39~3.30 Å). These multiple interactions shows a stronger interactions between SO<sub>2</sub> and SIFSIX-1-Cu.



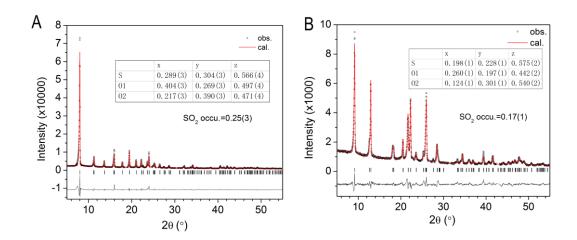
**Figure S12**. DFT-D calculated CO<sub>2</sub> binding sites in SIFSIX-3-Zn. Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Zn, violet; O, orange.

With a samll pore size of SIFSIX-3-Zn,  $CO_2$  were captured through four cooperative  $C^{\delta^+} \cdots F^{\delta^-}$  and multiple  $O^{\delta^-} \cdots H^{\delta^+}$  interactions. Adsorbed at the center of the one-dimensional channel (Figure S12), all of the four C $\cdots$ F distance were 3.36 Å.

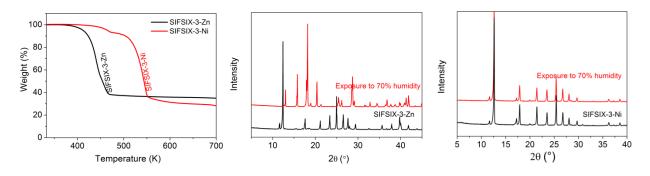


**Figure S13**. DFT-D calculated N<sub>2</sub> adsorption sites in SIFSIX-1-Cu (A), SIFSIX-3-Zn (B), and SIFISX-2-Cu-i (C). Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Cu, dark teal; Zn, violet; O, orange. (Note: the different nets of SIFSIX-2-Cu-i are highlighted in magenta and cyan for clarity).

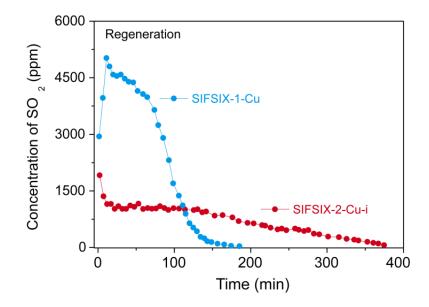
In addition, the calculated adsorption energy ( $\Delta E$ ) shows that there are much stronger interactions with SO<sub>2</sub> than CO<sub>2</sub> ( $\Delta E$  in SIFSIX-2-Cu-i, 50.2 versus 35.7 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-1-Cu, 50.3 versus 31.1 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-3-Zn, 54.1 versus 45.7 kJ mol<sup>-1</sup>). As for N<sub>2</sub>, the calculated  $\Delta E$  also shows that there are much stronger interactions with SO<sub>2</sub> than N<sub>2</sub> ( $\Delta E$  in SIFSIX-2-Cu-i, 50.2 versus 22.8 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-1-Cu, 50.3 versus 15.7kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-3-Zn, 54.1 versus 45.7 kJ mol<sup>-1</sup>).



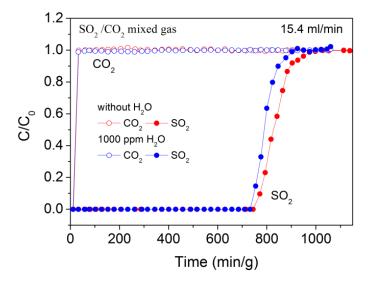
**Figure S14**. Powder X-ray diffraction patterns for the Rietveld refinement of SO<sub>2</sub>-loaded SIFSIX-1-Cu (A) and SO<sub>2</sub>-loaded SIFSIX-2-Cu-i (B). Goodness of fit data: (A)  $R_{wp} = 0.0891$ ,  $R_p = 0.0624$ ,  $\chi^2 = 3.96$ ; (B)  $R_{wp} = 0.0666$ ,  $R_p = 0.0492$ ,  $\chi^2 = 1.99$ .



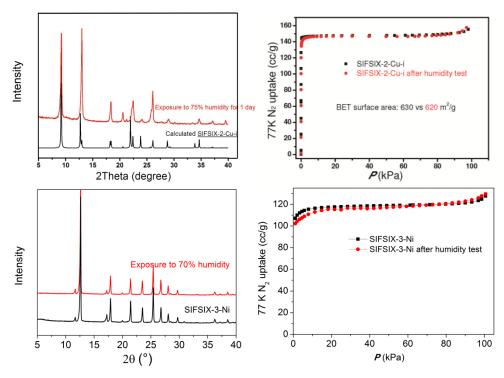
**Figure S15.** TGA patterns of sample SIFSIX-3-Zn and SIFSIX-3-Ni (A). XRD patterns of sample SIFSIX-3-Zn (B) and SIFSIX-3-Ni (C) after exposure to 75% humidity for 1 day.



**Figure S16.** Experimental desorption curves for SO<sub>2</sub> on SIFSIX-2-Cu-i ( $\Phi$ 4.6×50 mm, 0.21 g) and SIFSIX-1-Cu ( $\Phi$ 4.6×50 mm, 0.23 g) with He flow of 20 ml min<sup>-1</sup> at 313 K.



**Figure S17.** Experimental column breakthrough curves for  $SO_2/CO_2$  separations on SIFSIX-2-Cu-i ( $\Phi$ 4.6×50 mm, 0.21 g) at 298 K and 1.01 bar with the presence of moisture. The composition of the mixed gas: 1000 ppm H<sub>2</sub>O, 1870 ppm SO<sub>2</sub>, and 99.713% CO<sub>2</sub>.



**Figure S18.** XRD patterns of sample SIFSIX-2-Cu-i after exposure to 75% humidity for 1 day (A). The BET curves of fresh SIFSIX-2-Cu-i and the sample after exposure to 75% humidity for 1 day (B). XRD patterns of sample SIFSIX-3-Ni after exposure to 70% humidity for 5 days (C). The BET curves of fresh SIFSIX-3-Ni and the sample after exposure to 70% humidity for 5 days (D).<sup>[6]</sup>

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