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Selective recognition and dense packing of  $SO<sub>2</sub>$ clusters is achieved through multiple synergistic host-guest/guest-guest interactions within  $SiF_6^{2-}$  anion-pillared hybrid porous materials in article number 1606929, by Qiwei Yang, Banglin Chen, Huabin Xing, and co-workers. The binding sites of anions and aromatic rings on the pore surface grasp every atom of  $SO_2$ via  $S^{\delta+...}F^{\delta-}$  and  $O^{\delta-...}H^{\delta+}$  interactions, while the interactions between  $SO<sub>2</sub>$  molecules further promote the gas trapping.

# **GAS PURIFICATION**

**Gas Purification**



# **Ultrahigh and Selective SO<sub>2</sub> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials**

*Xili Cui, Qiwei Yang,\* Lifeng Yang, Rajamani Krishna, Zhiguo Zhang, Zongbi Bao, Hui Wu, Qilong Ren, Wei Zhou, Banglin Chen,\* and Huabin Xing\**

The efficient capture of SO<sub>2</sub> is of great significance in gas-purification pro**cesses including flue-gas desulfurization and natural-gas purification, but the design of porous materials with high adsorption capacity and selectivity of**  SO<sub>2</sub> remains very challenging. Herein, the selective recognition and dense packing of SO<sub>2</sub> clusters through multiple synergistic host-guest and guest**guest interactions by controlling the pore chemistry and size in inorganic anion (SiF6 <sup>2</sup><sup>−</sup>, SIFSIX) pillared metal–organic frameworks is reported. The binding sites of anions and aromatic rings in SIFSIX materials grasp every atom of SO2 firmly via S<sup>δ</sup><sup>+</sup>···F<sup>δ</sup><sup>−</sup> electrostatic interactions and O<sup>δ</sup><sup>−</sup>···H<sup>δ</sup><sup>+</sup>** dipole–dipole interactions, while the guest–guest interactions between SO<sub>2</sub> **molecules further promote gas trapping within the pore space, which is elucidated by first-principles density functional theory calculations and powder X-ray diffraction experiments. These interactions afford new benchmarks**  for the highly efficient removal of SO<sub>2</sub> from other gases, even if at a very low SO<sub>2</sub> concentration. Exceptionally high SO<sub>2</sub> capacity of 11.01 mmol g<sup>−1</sup> **is achieved at atmosphere pressure by SIFSIX-1-Cu, and unprecedented low-pressure SO<sub>2</sub> capacity is obtained in SIFSIX-2-Cu-i (4.16 mmol g<sup>−1</sup> SO<sub>2</sub> at 0.01 bar and 2.31 mmol g<sup>−1</sup> at 0.002 bar). More importantly, record SO<sub>2</sub>/** CO<sub>2</sub> selectivity (86–89) and excellent SO<sub>2</sub>/N<sub>2</sub> selectivity (1285–3145) are **also achieved. Experimental breakthrough curves further demonstrate the excellent performance of these hybrid porous materials in removing low**concentration SO<sub>2</sub>.

of low-grade fossil fuels.[3–6] Besides the direct detriment on environment and human health,  $SO_2$  will significantly inactivate the adsorbents or absorbents in removing  $CO<sub>2</sub>$  from flue gas although the concentration of  $SO_2$  in flue gas is very low (cat. 2000 ppm).[7,8] Moreover, in the reactions such as selective catalytic reduction of NO*x* and catalytic combustion of  $CH_{4}$ ,<sup>[9,10]</sup> even trace amount of  $SO_2$  could poison the catalysts and this deactivation is irreversible. The traditional flue-gas desulfurization (FGD) processes, with limestone or organic solvents as the absorbents,  $^{[11,12]}$  can remove about 90-95% SO<sub>2</sub>. However, these FGD technologies are energy-intensive and not efficient for the deep desulfurization. Therefore, there is an urgent demand for efficient technology to remove trace  $SO<sub>2</sub>$  in flue gas and other  $SO<sub>2</sub>$ -containing gases.

In the past decades, the development of energy-efficient physical-adsorption separation technology shows great potential in gas separation, which greatly motivates the design and synthesis of highly efficient porous materials.<sup>[13-15]</sup> Metal–organic frameworks (MOFs) and/ or porous coordination polymers are

Rapid economic growth all over the world has resulted in the excessive energy consumption as well as increasing environmental burdens.[1,2] One of the most serious related problems is the emission of sulfur dioxide  $(SO<sub>2</sub>)$ , induced by the utilization a class of hybrid porous materials composed of metal units joined by organic/inorganic linkers, in which the diversity of the organic/inorganic linkers and exquisite control over pore aperture size promise great potential for gas separation and purification.<sup>[16–18]</sup> However, compared to the separation of  $CO_2$ 

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and hydrocarbons,<sup>[19–29]</sup> the selective adsorption of  $SO<sub>2</sub>$  has rarely been studied on MOFs, especially the adsorption at low partial pressures that is actually needed by the gas desulfurization.<sup>[ $30-36$ ]</sup> Generally, the desulfurization of flue gas is a step before  $CO<sub>2</sub>$  scrubbing process, however, few work paid attention to the selective removal of  $SO_2$  from  $CO_2$ . In fact, considering the acidic nature of both  $SO_2$  and  $CO_2$  molecules and the much lower  $SO_2$  concentration in flue gas than  $CO_2$  (CO<sub>2</sub>: 10–12%, v/v; SO<sub>2</sub>: about 2000 ppm), it is very challenging to remove  $SO_2$ from  $CO<sub>2</sub>$  with high selectivity.<sup>[37,38]</sup> These abovementioned problems prompted us to develop advanced porous materials with delicate structure and chemistry for the adsorption of  $SO<sub>2</sub>$ , and elucidate the way in which contributions such as pore size and pore surface electrostatic environment enhance the selective recognition of  $SO<sub>2</sub>$  with high uptake capacity.

In this work, we for the first time reported the selective recognition and dense packing of the so-called "SO<sub>2</sub> cluster" using hybrid porous materials through precisely tuning the pore size and pore chemistry. Featuring copper coordination networks with inorganic hexafluorosilicate (SiF6<sup>2−</sup>, SIFSIX) anions and organic linkers, SIFSIX-1-Cu (1 = 4,4'-bipyridine)<sup>[24]</sup> and SIFSIX-2-Cu-i  $(2 = 4,4'-dipyridylacetylene, i = interpene$ trated)<sup>[19]</sup> contain pore spaces that enable high  $SO<sub>2</sub>$  uptake with specific recognition and afford new benchmarks for the highly efficient removal of  $SO<sub>2</sub>$  from other gases. Not only extraordinary ambient uptake of  $SO_2$  was achieved with SIFSIX-1-Cu as adsorbent, but also unprecedented low-pressure  $SO<sub>2</sub>$  capacity was attained with SIFSIX-2-Cu-i. Moreover, record  $SO<sub>2</sub>/CO<sub>2</sub>$ selectivity and excellent  $SO_2/N_2$  selectivity were also exhibited by the SIFSIX materials. We attribute this exceptional performance to the synergistic guest–host interactions ( $S^{\delta+}$  $\cdots$  $F^{\delta-}$  and  $O^{\delta-}\cdots H^{\delta+}$  interactions) that firmly grasp every atom of SO<sub>2</sub> in the pores of SIFSIX materials along with the considerable guest-guest interactions among  $SO<sub>2</sub>$  molecules and the optimal

pore size, which together enable the preferential binding and cluster formation of  $SO_2$  in the pores densely.

These SIFSIX materials exhibit a pillared square-grid 3D structure with inorganic  $\text{SiF}_6{}^{2-}$  ions as a linear bridge between transition-metal moieties. Previously, we have succeeded in the specific recognition of acetylene from ethylene using SIFSIX materials.[39] In this work, we systematically studied the adsorption of  $SO_2$  on SIFSIX-1-Cu, SIFSIX-2-Cu (2, 4,4'-dipyridylacetylene), SIFSIX-2-Cu-i, SIFSIX-3-Zn (3,pyrazine), and SIFSIX-3-Ni at atmospheric and low pressures. At first, the uptake capacity of  $SO_2$  as single-component gas on activated SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were determined at 298 K and 1.01 bar (**Table 1**). Remarkably, SIFSIX-1-Cu exhibited superb adsorption capacity (11.01 mmol g<sup>−</sup><sup>1</sup> ) among SIFSIX materials, while SIFSIX-2-Cu-i and SIFSIX-2-Cu uptake 6.90 and 6.50 mmol  $g^{-1}$ , respectively (Table 1). To the best of our knowledge, this extraordinarily high value of 11.01 mmol  $g^{-1}$  measured at room temperature and ambient pressure is the highest of all the materials reported under the same condition so far, including top-performing ones such as M(bdc)(ted)<sub>0.5</sub> (9.97 mmol g<sup>-1</sup>),<sup>[36]</sup> NOTT-300 (Al) (7.1 mmol g<sup>-1</sup>),<sup>[34]</sup> MFM-300(In) (8.28 mmol g<sup>-1</sup>),<sup>[35]</sup> and MFM-202a (10.2 mmol g−<sup>1</sup> ).[33]

The adsorption isotherms of  $SO<sub>2</sub>$  at 298 and 273 K on SIFSIX materials were measured to systematically demonstrate the  $SO<sub>2</sub>$ capture ability of these materials at low pressures (**Figure 1** and Table 1), as needed by the actual desulfurization process due to the low  $SO_2$  concentration in feed gas. Notably, the measurements were performed using  $SO_2/N_2$  mixed gas with varying SO<sub>2</sub> molar fractions under flow mode.

As can be noted from Figure 1A, the adsorption isotherms of SO2 on SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Ni, and SIFSIX-3-Zn show a steep increase in the low-pressure range and then reach saturation. At an extremely low  $SO_2$  partial pressure of

Table 1. The adsorption capacities of SO<sub>2</sub> in various porous materials at different partial pressure of SO<sub>2</sub>. Summary of the adsorption collected at 298 K. Note: The SO<sub>2</sub> adsorption capacities at 0.002, 0.01, and 0.1 bar were determined using SO<sub>2</sub>/N<sub>2</sub> mixed gas with varying SO<sub>2</sub> molar fractions under flow mode, while the  $SO_2$  adsorption capacities at 1.0 bar were determined using  $SO_2$  pure gas.

Materials	$SO2$ uptake [mmol $g^{-1}$ ]				Selectivity for SO <sub>2</sub> /CO <sub>2</sub> at 10/90 mixture	Selectivity for $SO_2/N_2$ at 10/90 mixture	Selectivity for SO <sub>2</sub> /CH <sub>4</sub> at 10/90 mixture	$Q_{\rm st}$ $[SO_2 \, k] \, mol^{-1}]$
	$0.002$ bar <sup>a)</sup>	$0.01$ bar <sup>a)</sup>	$0.1$ bar <sup>a)</sup>	1.0 <sub>bar</sub>				
SIFSIX-1-Cu	1.80	3.43	8.74	11.01	70.7	3145.7	1241.4	36.1
SIFSIX-2-Cu-i	2.31	4.16	6.01	6.90	87.1	3103.2	1017.1	38.1
SIFSIX-3-Zn	0.98	1.68	1.89	2.10		506.7	276.0	45.2
SIFSIX-3-Ni	1.39	2.43	2.55	2.74		701.8	371.6	43.2
SIFSIX-2-Cu			-	6.50		-		
$Ni(bdc) (ted)_{0.5}$ [36]	$\qquad \qquad -$	$\overline{\phantom{m}}$	3.50	9.97				
Zn-MOF-74[30]	-	$3.03^{b}$	-	$\overline{\phantom{0}}$				
MFM-300(In) <sup>[35]</sup>	$\qquad \qquad -$		-	8.28	50 <sup>d</sup>	2700 <sup>d</sup>	$\qquad \qquad -$	$34.5/39.6$ <sup>e)</sup>
MFM-202a <sup>[33]</sup>			3.0	10.2				35
NOTT-300 (Al) <sup>[34]</sup>				7.1 <sup>f</sup>				
P(TMGA-co-MBA) <sup>[40]</sup>	$\qquad \qquad -$			4.06				
Activated Carbon <sup>[41]</sup>	$\overline{\phantom{0}}$			3.3c				

<sup>a)</sup>Partial pressure of SO<sub>2</sub>; <sup>b</sup>)Dynamic adsorption capacity; <sup>c)</sup>At the temperature of 323 K and pressure of 0.46 bar; <sup>d)</sup>These data were read from the figures of ref. [35];<br><sup>e)</sup>Highest Q<sub>st</sub> values at different surfa







Figure 1. A) SO<sub>2</sub> adsorption isotherms of SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni at 273 and 298 K. Adsorption isotherms for SO<sub>2</sub>,  $CO<sub>2</sub>$ , CH<sub>4</sub> and N<sub>2</sub> on B) SIFSIX-1-Cu, C) SIFSIX-2-Cu-i, and D) SIFSIX-3-Ni at 298 K. Note: SO<sub>2</sub> isotherms were measured using SO<sub>2</sub>/N<sub>2</sub> mixed gas with varying SO<sub>2</sub> molar fractions under flow mode. CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> isotherms were measured using single-component gas. IAST selectivities of SIFSIX materials with E)  $SO_2/CO_2$  mixtures and F)  $SO_2/N_2$  mixtures with varying  $SO_2$  molar fractions in gas phase at 100 kPa.

0.002 bar (2000 ppm) and 298 K, SIFSIX-2-Cu-i rapidly uptake as high as 2.31 mmol  $g^{-1}$  SO<sub>2</sub> (Figure 1C and Table 1), exceeding the capacity of SIFSIX-1-Cu (1.80 mmol g−<sup>1</sup> ), SIFSIX-3-Zn (0.98 mmol g−<sup>1</sup> ), and SIFSIX-3-Ni (1.39 mmol g−<sup>1</sup> ) (Figure 1B,D and Table 1). This excellent capacity of  $SO_2$  at such a low pressure indicates that SIFSIX-2-Cu-i has great potential in FGD applications. At 298 K, when the partial pressure of  $SO_2$ increased to  $0.01$  bar, the  $SO<sub>2</sub>$  uptake of SIFSIX-2-Cu-i rose to 4.16 mmol g−<sup>1</sup> SO2, not only still higher than the other three SIFSIX materials but also exceeding the benchmark uptake of Zn-MOF-74 (3.03 mmol  $g^{-1}$ ). As the pressure of SO<sub>2</sub> further increased to 0.1 bar, the uptake amount of  $SO_2$  at 298 K on SIFSIX-1-Cu increased more rapidly and became more than that on SIFSIX-2-Cu-i, approaching a value of 8.74 mmol  $g^{-1}$ while SIFSIX-2-Cu-i exhibits 6.01 mmol g<sup>-1</sup>, both higher than that ever reported under the same conditions  $(3.5 \text{ mmol g}^{-1}$  by Ni(bdc)(ted)<sub>0.5</sub>). When the temperature decreased to 273 K, a steep increase in the low-pressure range of isotherms to a high  $SO<sub>2</sub>$  capacity was still observed on all these five SIFSIX materials. As shown in Figure 1A, at 273 K and the low  $SO_2$  partial pressure of 0.002 bar, SIFSIX-2-Cu-i exhibited remarkable higher uptake of SO<sub>2</sub> (3.72 mmol g<sup>-1</sup>), exceeding SIFSIX-1-Cu  $(3.18 \text{ mmol g}^{-1})$  and SIFSIX-3-Ni  $(2.34 \text{ mmol g}^{-1})$ . With the increase of  $SO_2$  partial pressure, SIFSIX-1-Cu exhibited higher uptake than SIFSIX-2-Cu-i, SIFSIX-3-Ni, and SIFSIX-3-Zn within the whole range of 0.01–1.01 bar. Overall, the results in Table 1 and Figure 1A demonstrate that exceptional  $SO<sub>2</sub>$ capacity can be afforded by SIFSIX materials from atmospheric to very low pressures, even more superior at low pressures.

To evaluate the selectivity of  $SO<sub>2</sub>$  to other typical gases in gas desulfurization processes, adsorption isotherms of  $CO<sub>2</sub>$ ,  $CH<sub>4</sub>$ ,

and  $N_2$  on SIFSIX materials were collected at 298 K using pure gas. Although both  $CO<sub>2</sub>$  and  $SO<sub>2</sub>$  are acidic gases, the  $CO<sub>2</sub>$  isotherms on SIFSIX-1-Cu show dramatically different adsorption behaviors than  $SO_2$  adsorption isotherms (Figure 1B,C). These dramatic differences between  $SO_2$  and  $CO_2$  adsorption behavior and capacity, especially at low pressures, offer a great potential of selective recognition of  $SO_2$  toward  $CO_2$  on SIFSIX-1-Cu and SIFSIX-2-Cu-i. In addition, SIFSIX-1-Cu and SIFSIX-2- Cu-i only adsorbed 0.45 and 0.55 mmol g<sup>-1</sup> CH<sub>4</sub> at 298 K and 1.0 bar (Figure 1A,B), respectively, which are negligible compared to  $SO<sub>2</sub>$  uptake capacity. Furthermore, the uptake amount of  $N_2$  was much lower than CH<sub>4</sub> (Figure 1B–D). As for the case of SIFSIX-3-Ni (Figure 1D) and SIFSIX-3-Zn (Figure S4, supporting information), the  $CO<sub>2</sub>$  capacity was higher than the  $SO<sub>2</sub>$ capacity, and  $CH_4$  and  $N_2$  were still rarely adsorbed.

In order to further address the separation capability of SIFSIX materials in different gas desulfurization processes,  $SO<sub>2</sub>/CO<sub>2</sub>$  and  $SO<sub>2</sub>/N<sub>4</sub>$  separation selectivity were determined using ideal adsorbed solution theory (IAST) calculations as a function of varying  $SO_2$  composition (from 0.1 to 0.9).<sup>[42,43]</sup> Notably, in these IAST calculations, the  $SO_2$  isotherms on SIFSIX materials were measured using  $SO_2/N_2$  mixed gas, which might slightly underestimate the selectivity. As shown in Figure 1E, SIFSIX-1-Cu shows excellent  $SO_2/CO_2$  separation selectivity (54–70) over a wide range of  $SO_2$  molar fraction in gas phase (0.1–0.9), especially in the low concentration range. Even better, SIFSIX-2-Cu-i exhibits record  $SO<sub>2</sub>/CO<sub>2</sub>$  selectivity (86–89) within 0.1–0.9 molar fraction of  $SO<sub>2</sub>$ . Considering the fact of low  $SO_2$  concentration in typical flue gas  $(SO_2/CO_2/N_2)$ , this large  $SO_2/CO_2$  selectivity endows SIFSIX-1-Cu and SIFSIX-2-Cu-i with potential in FGD process. This is crucial to realize a thorough removal of trace  $SO<sub>2</sub>$  from flue gas before the  $CO<sub>2</sub>$ scrubbing process to ensure the activity of  $CO<sub>2</sub>$  adsorbent. To the best of our knowledge, the  $SO<sub>2</sub>/CO<sub>2</sub>$  IAST selectivity on SIFSIX-2-Cu-i (86–89) and SIFSIX-1-Cu (54–70) sets new benchmarks for  $SO<sub>2</sub>/CO<sub>2</sub>$  separation. The separation selectivities of  $SO<sub>2</sub>/N<sub>2</sub>$  and  $SO<sub>2</sub>/CH<sub>4</sub>$  on the SIFSIX materials were as well estimated by IAST. Figure 1 F shows the high  $SO_2/N_2$  selectivities on SIFSIX-1-Cu (2510–3145) and SIFSIX-2-Cu-i (1285–3103) over a wide range of  $SO_2$  molar fraction in gas phase (0.1–0.9). Moreover, high  $SO_2/CH_4$  selectivities (Figure S5, Supporting Information) over the same range of  $SO<sub>2</sub>$  molar fraction were also achieved on SIFSIX-1-Cu (992–1241), SIFSIX-2-Cu-i (422–1017), and SIFSIX-3-Ni (86–371). Therefore, SIFSIX-1-Cu and SIFSIX-2-Cu-i fulfill the requirements by FGD technology, natural-gas purification and other  $SO_2$ -separation processes for both  $SO<sub>2</sub>$  capacity and selectivity.

To unravel the nature of the interactions between  $SO<sub>2</sub>$  molecule and SIFSIX materials, we performed modeling studies using first-principles DFT-D (dispersion-corrected density functional theory) calculations. When trapped within the pore of SIFSIX-1-Cu,  $SO_2$  gets adsorbed primarily through the S<sup>δ+</sup>···F<sup>δ−</sup> electrostatic interaction (**Figure 2**) with SiF<sub>6</sub><sup>−</sup> anion and the multiple  $O^{\delta-}\cdots H^{\delta+}$  dipole–dipole interactions with the 4,4′-bipyridine linker (Figure 2B). The DFT-D calculated S $\cdots$ F distance is ≈2.6 Å (Figure 2A), much smaller than the sum of the van der Waals radii of S and F (3.3 Å), indicating the considerable strength of this interaction that arises from the negative nature of  $\text{SiF}_6{}^{2-}$  ion and positive charge of S atom. Simultaneously, the two oxygen atoms of  $SO<sub>2</sub>$  molecule are bonded by the 4,4′-bipyridine linker through multiple dipole– dipole interactions, especially the  $O^{\delta-}\cdots H^{\delta+}$  interactions between oxygen atoms and aromatic hydrogens with a distance of 2.39–3.30 Å (Figure 2B). These multiple synergistic interactions enable the specific recognition of  $SO<sub>2</sub>$  molecules through grasping every atoms of the adsorbed  $SO_2$ , with a calculated strong adsorption energy (ΔE) of 50.3 kJ mol<sup>-1</sup>. Thanks to the four equivalent F sites and four equivalent aromatic linkers, four SO2 molecules were trapped firmly by the host–guest  $S^{\delta \dagger}$ ····F $\delta$  and  $O^{\delta \dagger}$ ·····H $\delta \dagger$  interactions per unit cell. After that, it is noticed that there are still occupiable pore space in the unit

cell of SIFSIX-1-Cu (between the F sites, along crystallography  $c$  direction) to accommodate more  $SO_2$  guests. DFT-D calculations showed that two more  $SO<sub>2</sub>$  molecules could be trapped in this space as the secondary adsorption, through the dipole– dipole interactions with the channel pore surface and the intermolecular interaction (mainly dipole–dipole interaction) with the SO<sub>2</sub> adsorbed at the primary sites. The  $\Delta E$  of SO<sub>2</sub> on this site was 38.7 kJ mol<sup>-1</sup>, with a calculated nearest S<sub>site2</sub>···O<sub>site1</sub> distance of 3.6 Å. As a result, six  $SO_2$  were trapped within per unit cell of SIFSIX-1-Cu, four of which were primarily adsorbed via host–guest interactions and the other two were secondarily accommodated mainly via guest–guest interaction with the primary SO<sub>2</sub>.

Previous studies have shown that the intermolecular distance in  $SO_2$  liquid tested from X-ray diffraction and neutron studies were centered at 3.5, 4.5, and 5.6 Å with different types of orientations.[44,45] As clearly shown in Figure 2A, the intermolecular distance of adsorbed  $SO_2(I)$  and  $SO_2(II)$  is 3.32, 3.56, and 4.07 Å, respectively, within the distance range of the liquid  $SO<sub>2</sub>$ . These abovementioned data visualize the dense packing of " $SO<sub>2</sub>$  clusters" within the confined electrostatic nanospace of SIFSIX-1-Cu, in consequence of the synergistic host–guest and guest–guest interactions. It is worth noting that this dense packing of "SO<sub>2</sub> clusters" at ambient temperature and low pressure has rarely been reported in common porous adsorbents.

The dense packing of  $SO<sub>2</sub>$  clusters within SIFSIX materials is not only the result of the unique pore chemistry but also the optimal pore size. When the organic linker in SIFSIX-1-Cu was replaced by a longer analog, 4,4′-dipyridylacetylene, the resulted SIFSIX-2-Cu showed a weaker interaction with SO2 (44.2 kJ mol<sup>−</sup><sup>1</sup> ) than SIFSIX-1-Cu. The S···F electrostatic interaction was basically of the same nature and strength in the two isoreticular MOFs, implied by the very similar  $S \cdots F$ distances, but the dipole–dipole interaction between  $SO_2$  and the 4,4′-dipyridylacetylene linker was slightly weaker than the 4,4′-bipyridine case because of the larger channel pore size of this SIFSIX material. The experimental  $SO<sub>2</sub>$  capacity of SIFSIX-2-Cu at room temperature and 1 bar was 6.5 mmol  $g^{-1}$ , equivalent to ≈3.7 SO<sub>2</sub> per unit cell. This is lower than the capacity of SIFSIX-1-Cu that was 11.0 mmol g−<sup>1</sup> and equivalent to



Figure 2. A,B) DFT-D calculated SO<sub>2</sub> adsorption binding sites in SIFISX-1-Cu viewing in two different directions. Color code: F, red; Si, light blue; C, gray; H, light gray; N, sky blue; Cu, dark teal; O, orange; S, sea green (Note: the secondary adsorbed SO<sub>2</sub> molecules were highlighted with bright color).







Figure 3. A,B) DFT-D calculated SO<sub>2</sub> adsorption binding sites in SIFISX-3-Zn viewing in two different directions. Color code: F, red; Si, light blue; C, gray; H, light gray; N, sky blue; Zn, violet; O, orange; S, sea green.

 $\approx$ 5.7 SO<sub>2</sub> per unit cell. A too small pore size also goes against the uptake of  $SO_2$ . In SIFSIX-3-Zn, the channel pore size is small due to the much shorter linker pyrazine. DFT-D calculations show that  $SO<sub>2</sub>$  molecules get preferentially adsorbed at the center of the 1D channel of SIFSIX-3-Zn along the crystallography  $c$ -axis. Although the calculated  $\Delta E$  of SO<sub>2</sub> with SIFSIX-3-Zn was 54.1 kJ mol<sup>-1</sup>, slightly higher than that in SIFSIX-1-Cu, the much smaller pore volume captured less  $SO_2$  than SIFSIX-1-Cu. The much longer S···F distance (3.60 Å) demonstrates a weaker  $S^{\delta \dagger} \cdots F^{\delta}$  interaction between  $SO_2$  and SIFSIX-3-Zn (**Figure 3**) than the SIFSIX-1-Cu case, and the grasp of one  $SO<sub>2</sub>$  in SIFSIX-3-Zn consumes four times as much F sites as in SIFSIX-1-Cu.

The significance of a well-designed pore chemistry and pore size on the dense packing of  $SO_2$  clusters was further highlighted by the modeling on SIFSIX-2-Cu-i. Although the organic linker in SIFSIX-2-Cu-i is the same as that in SIFSIX-2-Cu, the framework interpenetration in SIFSIX-2-Cu-i enables the size of its unit cell approximately half of that of SIFSIX-2-Cu with a more compact SiF6 <sup>2</sup><sup>−</sup> distribution (**Figure 4**). DFT-D calculation showed that the S···F distance in this MOF is ≈2.44 Å, lower than those in other modeled SIFSIX materials, indicating a strong  $S^{\delta \dagger} \cdots F^{\delta}$  electrostatic interaction between  $SO_2$ and  $\text{SiF}_6^2$ -. On the other hand, the two O atoms of  $\text{SO}_2$  interact with the H atoms of 4,4′-dipyridylacetylene through multiple

O<sup>δ</sup>−···H<sup>δ</sup>+ interactions, with O···H distances of 2.79–3.34 Å (Figure 4A). In consequence, every atom of the adsorbed  $SO_2$ was grasped by the pore surface of SIFSIX-2-Cu-i through these multiple synergistic host–guest interactions, with a Δ*E* of ≈50.2 kJ mol−<sup>1</sup> . This is comparable to that in SIFSIX-1-Cu (≈50.3 kJ mol<sup>-1</sup>). The two SiF<sub>6</sub><sup>2-</sup> anions on the diagonal of each unit cell in SIFSIX-2-Cu-i enables the adsorption of two  $SO<sub>2</sub>$  by the host–guest  $S^{\delta \dagger} \cdots F^{\delta}$  and  $O^{\delta \dagger} \cdots H^{\delta \dagger}$  interactions. Interestingly, because those two  $SO_2$  molecules are located very close to each other, with the nearest S ··· O distance of only ≈3.2 Å, which enhance the guest–guest interactions (Figure 4A,B). The cooperation of the host–guest and guest–guest interactions affords the formation of  $SO<sub>2</sub>$  clusters within the confined electrostatic nanospace of SIFSIX-2-Cu-i. The nearest S···O distance of ≈3.2 Å between two neighboring adsorbed SO<sub>2</sub> is comparable to the intermolecular distance (3.5–5.6 Å) in liquid crystal  $SO_2$  phase and even slightly smaller than that in SIFSIX-1-Cu, implying a dense packing of  $SO<sub>2</sub>$  clusters within the pores of SIFSIX-2-Cu-i that enables the excellent uptake of  $SO<sub>2</sub>$  at low partial pressures. As presented in Table 1, the experimental  $SO<sub>2</sub>$ adsorption capacity of SIFSIX-2-Cu-i at room temperature and 0.01 bar was as large as 4.16 mmol g<sup>-1</sup>, much higher than those in SIFSIX-1-Cu (3.43 mmol g−<sup>1</sup> ), SIFSIX-3-Zn and SIFSIX-3-Ni. Even if at 0.002 bar (2000 ppm) the  $SO<sub>2</sub>$  capacity was as high as 2.26 mmol g−<sup>1</sup> . Overall, DFT-D calculations on the different



Figure 4. A,B) DFT-D calculated SO<sub>2</sub> adsorption sites in SIFISX-2-Cu-i viewing in two different directions, and C) crystal structure obtained from Rietveld refinement of PXRD data on SO2-loaded SIFSIX-2-Cu-i. (Note: the different nets are highlighted in magenta and cyan for clarity).





Figure 5. A,B) Crystal structure obtained from Rietveld refinement of PXRD data on SO<sub>2</sub>-loaded SIFSIX-1-Cu (A) and SIFSIX-2-Cu-i (B).

SIFSIX materials manifest that the excellent  $SO<sub>2</sub>$  capture performance of SIFSIX-1-Cu and SIFSIX-2-Cu-i can be attributed to the synergetic host–guest binding (electrostatic and dipole– dipole interactions) and cooperative guest–guest interactions within the confined electrostatic nanospace of moderate size to form  $SO<sub>2</sub>$  clusters.

To provide experimental proof for the DFT-D analysis of  $SO<sub>2</sub>$ -SIFSIX interactions, we have performed Rietveld refinement of the powder X-ray diffraction patterns of  $SO<sub>2</sub>$ -loaded samples to locate the adsorbed positions of  $SO<sub>2</sub>$  molecules in the crystal structure of SIFSIX materials, and the experimental results are well consistent with the DFT-D calculation results. The Rietveld refined data reveals that in the interpenetrated structure of SIFSIX-2-Cu-i, each SO<sub>2</sub> molecule indeed interacts with SIFSIX-2-Cu-i through  $S^{\delta_+}\cdots F^{\delta_-}$  bonding (2.52 Å) and multiple  $O^{\delta_-}\cdots H^{\delta_+}$  interactions (**Figure** 5B). The nearest S $\cdots$ O distance between adjacent SO<sub>2</sub> molecules are 3.2 Å. In SIFSIX-1-Cu,  $SO_2$  also gets adsorbed primarily through the  $S^{\delta \cdot \cdot \cdot}$   $F^{\delta \cdot}$  electrostatic interaction with  $\text{SiF}_6$ <sup>-</sup> anion (Figure 5A). The  $S^{\delta +} \cdots F^{\delta -}$  distance is 3.04 Å, longer than the modeling results (2.61 Å). Cooperative interactions between adjacent  $SO<sub>2</sub>$  molecules are also observed in the crystal structure of SIFSIX-1-Cu-SO<sub>2</sub> with a S $\cdots$ O distance of 3.3 Å.

We also have performed the detailed DFT-D calculations for  $CO<sub>2</sub>/N<sub>2</sub>$  molecules to illustrate the difference on interactions between  $SO_2$  and  $N_2/CO_2$  molecules. Results show that the calculated C $\cdots$ F distances between CO<sub>2</sub> and SiF<sub>6</sub><sup>2-</sup> (2.52 and 2.80 Å) in SIFSIX-2-Cu-i (Figure S10, Supporting Information) are longer than those between  $SO_2$  and  $SiF<sub>6</sub><sup>2–</sup> binding$ sites (2.44 Å), indicating that SIFSIX-2-Cu-i interacted more strongly with  $SO_2$  than  $CO_2$ . In SIFSIX-1-Cu, the calculated C $\cdots$ F distance for CO<sub>2</sub> (2.60 Å) is comparable to the S $\cdots$ F distance for SO<sub>2</sub> (2.61 Å); however, the calculated  $O \cdots H$  distances between  $CO_2$  molecule and 4,4'-bipyridine (2.64–3.58 Å) are longer than that of  $SO_2$  system (2.39–3.30 Å) (Figure S11, Supporting Information). Additionally, the static adsorption energy  $(\Delta E)$  results show that there are much stronger interactions with  $SO_2$  than  $CO_2$  ( $\Delta E$  in SIFSIX-2-Cu-i, 50.2 versus 35.7 kJ mol−<sup>1</sup> ; Δ*E* in SIFSIX-1-Cu, 50.3 vs 31.1 kJ mol−<sup>1</sup> ; Δ*E* in SIFSIX-3-Zn, 54.1 versus 45.7 kJ mol<sup>−</sup>1).

To confirm the actual  $SO_2/N_2$  and  $SO_2/CO_2$  separation performance on the SIFSIX materials, we conducted experimental breakthrough tests at 298 K and 1.01 bar on SIFSIX-2-Cu-i, SIFSIX-1-Cu, and SIFSIX-3-Ni (Figure 6). SO<sub>2</sub>/N<sub>2</sub> mixture containing 2000 ppm  $SO_2$  was used to mimic the flue gas with low concentration of  $SO<sub>2</sub>$ . The reason for using SIFSIX-3-Ni rather than SIFSIX-3-Zn is the relatively higher stability of SIFSIX-3-Ni (Figure S15, Supporting Information). As shown in Figure 6A, highly efficient elimination of  $SO<sub>2</sub>$  was achieved with clean  $N_2$  eluted from the bed by all the three SIFSIX materials. The breakthrough time of  $SO<sub>2</sub>$  on SIFSIX-2-Cu-i (1800 min g−<sup>1</sup> ) exceeded that on SIFSIX-1-Cu and SIFSIX-3-Ni, consistent with the higher  $SO<sub>2</sub>$  adsorption capacities of SIFSIX-2-Cu-i (2.31 mmol  $g^{-1}$ ) than SIFSIX-1-Cu (1.80 mmol  $g^{-1}$ ) and SIFSIX-3-Ni (1.39 mmol g−<sup>1</sup> ) in static adsorption experiment at 298 K and 0.002 bar (Figure 1A). Additionally, the actual  $SO_2/CO_2$ separation performance on these SIFSIX materials was also confirmed by the breakthrough experiments, in which the  $SO<sub>2</sub>/CO<sub>2</sub>$ mixture containing 2000 ppm  $SO_2$  was used. As shown in Figure 6B, outstanding efficient separation of  $SO_2/CO_2$  was achieved with clean  $CO<sub>2</sub>$  eluted from the bed by SIFSIX-1-Cu and SIFSIX-2-Cu-i, agreeing well with the results of adsorption isotherm and IAST calculations. The superb  $SO_2/N_2$  and  $SO_2/CO_2$  selectivity at very low  $SO<sub>2</sub>$  concentrations makes SIFSIX materials very promising for the gas desulfurization applications.

Given that  $SO_2$  is highly corrosive and few porous MOF materials are stable to the presence of  $SO_2$ , concerns about material regeneration are raised. Therefore, we conducted cycling breakthrough tests to evaluate the reusability of SIFSIX-2-Cu-i and SIFSIX-1-Cu for  $SO<sub>2</sub>$  capture. As the desorption curves shown in the Figure S16 (Supporting Information), SIFSIX materials adsorbed with  $SO<sub>2</sub>$  could be fully regenerated by He flow at 313 K. The breakthrough performance of SIFSIX-2-Cu-i and SIFSIX-1-Cu for  $0.2/99.8$  (SO<sub>2</sub>/CO<sub>2</sub>) mixture did not declined during 6 and 4 cycles, respectively (Figure 6C,D). And XRD patterns indicated that both of the SIFSIX materials retain their stability after breakthrough experiments (Figure S6, Supporting Information). In addition, moisture (1000 ppm) has slightly effect on the adsorption capacity of SO<sub>2</sub> on SIFSIX-2-Cu-i (Figure S17, Supporting Information) and SIFSIX-2-Cu-i is stable when exposed to humidity (75%) (Figure S18, Supporting Information).

In summary, this work reports the selective recognition and dense packing of the so-called  $SO<sub>2</sub>$  clusters in hybrid porous materials with inorganic-anion-pillared metal–organic framework for the first time. The multiple binding sites of anionic and aromatic linkers initiate the specific recognition of  $SO_2$ by host-guest interactions that grasp the every atom of  $SO_2$ 





Figure 6. A,B) Experimental column breakthrough curves for SO<sub>2</sub>/N<sub>2</sub> (2000 ppm SO<sub>2</sub>) separations with SIFSIX-1-Cu, SIFSIX-2-Cu-i, and SIFSIX-3-Ni, and SO<sub>2</sub>/CO<sub>2</sub> (2000 ppm SO<sub>2</sub>) separations (A) and with SIFSIX-1-Cu and SIFSIX-2-Cu-i (B) at 298 K and 1.01 bar. C,D) Cycling column breakthrough tests for CO<sub>2</sub>/SO<sub>2</sub> (2000 ppm SO<sub>2</sub>) separations with SIFSIX-2-Cu-i (C) and SIFSIX-1-Cu (D) at 298 K and 1.01 bar (mixed gas flow: 14 mL min<sup>-1</sup>). In panel (A), open circles are for N<sub>2</sub>, and filled circles are for SO<sub>2</sub>. In panel (B), the open circles are for CO<sub>2</sub>, and the filled circles are for SO<sub>2</sub>.  $C_A/C_0$ , outlet concentration/feed concentration.

firmly, while the dipolar guest–guest interactions between  $SO_2$ molecules enforce the adsorption through promoting the primary binding and enabling secondary adsorption to form  $SO<sub>2</sub>$ clusters. A moderate pore size is crucial to afford adequate strength of synergistic host–guest and guest–guest interactions for a dense packing of  $SO_2$ . Thanks to the suitable pore chemistry and size, SIFSIX-1-Cu showed exceptionally high adsorption capacity of  $SO_2$  (11.01 mmol  $g^{-1}$  at 1.01 bar) and selectivity SIFSIX-2-Cu-i exhibited unprecedented  $SO_2$  capacity at low pressures (4.16 mmol  $g^{-1}$  at 0.01 bar and 2.31 mmol  $g^{-1}$  at 0.002 bar) and record  $SO_2/CO_2$  selectivity (86–89), while SIFSIX-1-Cu showed exceptionally high adsorption capacity of  $SO<sub>2</sub>$  (11.01) mmol  $g^{-1}$ ) at 1.01 bar and also excellent  $SO_2/CO_2$  selectivity (54–70). Additionally, extraordinarily high  $SO<sub>2</sub>/N<sub>2</sub>$  selectivity was also achieved by SIFSIX-2-Cu-i (1285–3103) and SIFSIX-1-Cu (2510–3145). As further confirmed by the breakthrough experiments for mixed gases containing 2000 ppm  $SO_2$ , this excellent performance sets a new benchmark in the highly efficient elimination of  $SO_2$  from flue gas or natural gas even if with a low  $SO<sub>2</sub>$  concentration, and this work will be also instructive for the design of porous materials for other gas-purification processes.

#### **Experimental Section**

*Materials*: SIFSIX materials including SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were synthesized as previously described in refs. [19] and [24] (see the Supporting Information for details).[19,24]

*SO2 Adsorption*: SO2 adsorption isotherms at 298 and 273 K were collected using the apparatus in Figure S1 (Supporting Information). Activated samples were packed in a glass container which was partly immersed in a water bath. The  $SO_2$  adsorption isotherms were determined using  $SO_2/N_2$  mixed gas with varying  $SO_2$  molar fractions under flow mode. Note: the adsorption of  $SO_2$  at 1.01 bar was measured with pure  $SO_2$  at flow mode. At the beginning of this experiment, the activated sample was loaded in the glass container which was full of pure  $N_2$  atmosphere at 760 mmHg. Then, the  $SO_2/N_2$  mixed gas (e.g., 0.002/99.998) was introduced at a constant flow at 760 mmHg. Adsorption equilibrium was reached until the weight of glass container kept constant and did not change. The  $SO<sub>2</sub>$  uptake was calculated based on the weight change before and after dynamic adsorption (see the Supporting Information for more detailed adsorption procedures).

*Breakthrough Tests*: The breakthrough experiments were carried out in a dynamic gas breakthrough equipment (see Figure S2 in the Supporting Information).[39] All experiments were conducted using a stainless steel column (4.6 mm inner diameter  $\times$  50 mm). According to the different particle size and density of the sample powder, the weight packed in the column was: SIFSIX-1-Cu powder (0.21 g), SIFSIX-2-Cu-i (0.21 g), and SIFSIX-3-Ni (0.50 g), respectively. The column packed with sample was first purged with He flow (15 mL min−<sup>1</sup> ) for 12 h at room temperature (25 °C). The mixed gas of  $SO_2/N_2 = 0.2/99.8$  (v/v) was then introduced at 21 mL min<sup>-1</sup>, and  $SO_2/CO_2 = 0.2/99.8$  (v/v) was introduced at 14 mL min<sup>−</sup><sup>1</sup> . Outlet gas from the column was monitored using gas chromatography (GC-2010 plus) with a thermal conductivity detector (TCD) coupled with a FID. The gas mixture was separated by a capillary column (Agilent GS-GASPRO,  $\Phi$ 0.32  $\times$  60 m). The concentration of  $SO_2$ ,  $CO_2$  or  $N_2$  in the outlet gas was monitored by the TCD. After the





breakthrough experiment, the sample was regenerated with He flow (7 to 15 mL min−<sup>1</sup> ) for 6–20 h.

*Density-Functional Theory Calculations*: First-principles densityfunctional theory (DFT) calculations were performed using the Quantum-Espresso package. A semi-empirical addition of dispersive forces to conventional DFT was included in the calculation to account for van der Waals interactions.<sup>[46]</sup> Vanderbilt-type ultrasoft pseudopotentials and generalized gradient approximation with Perdew–Burke–Ernzerhof exchange correlation were used. A cutoff energy of 544 eV and a  $2 \times 2 \times 4$  k-point mesh (generated using the Monkhorst–Pack scheme) were found to be enough for the total energy to converge within 0.01 meV atom<sup>−</sup>1. The structure of SIFSIX MOFs was first optimized. The optimized structures are good matches for the experimentally determined crystal structures of the coordination networks. Various guest gas molecules were then introduced to various locations of the channel pore, followed by a full structural relaxation. To obtain the gas binding energy, an isolated gas molecule placed in a supercell (with the same cell dimensions as the MOF crystal) was also relaxed as a reference. The static binding energy (at  $T = 0$  K) was then calculated using:  $E_{\text{B}} = E(\text{MOF}) + E(\text{gas}) - E(\text{MOF} + \text{gas}).$ 

*Fitting of Isotherms*: The isotherm data for  $SO_2$ ,  $CO_2$ ,  $CH_4$ , and  $N_2$  in SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were fitted with either the Langmuir–Freundlich isotherm model:

$$
q = q_{\text{sat}} \frac{bp^{\nu}}{1 + bp^{\nu}}
$$
 (1)

with *T*-dependent parameters *b*:

$$
b = b_0 \exp\left(\frac{E}{RT}\right) \tag{2}
$$

*IAST Calculations of Adsorption Selectivities*: The adsorption selectivity for  $C_2H_2/C_2H_4$  separation is defined by:

$$
S_{ads} = \frac{q_1/q_2}{p_1/p_2} \tag{3}
$$

*where*  $q_1$  and  $q_2$  are the molar loadings in the adsorbed phase in equilibrium with the bulk gas phase with partial pressures  $p_1$ , and  $p_2$ .

#### **Supporting Information**

Supporting Information is available from the Wiley Online Library or from the author.

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#### **Conflict of Interest**

The authors declare no conflict of interest.

#### **Keywords**

adsorption, gas purification, ionic hybrid porous materials,  $SO<sub>2</sub>$  cluster, sulfur dioxide

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# **ADVANCED<br>MATERIALS**

# Supporting Information

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Ultrahigh and Selective SO<sub>2</sub> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials

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# Supporting Information

#### **Ultrahigh and Selective SO<sup>2</sup> Uptake in Inorganic Anion-Pillared Hybrid Porous Materials**

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Materials and Methods

Tables S1-S6

Figures. S3 to S18

#### **Experiments**

#### *Materials*

Ammonium hexafluorosilicate  $((NH)_2\text{SiF}_6, 98\%,$  Aldrich), copper  $(II)$  tetrafluoroborate hydrate (Cu(BF<sub>4</sub>)<sub>2</sub>• xH<sub>2</sub>O, 98%, Aldrich), zinc hexafluorosilicate hydate (ZnSiF<sub>6</sub>• xH<sub>2</sub>O, 99%, Aldrich), 4,4'-bipyridine  $(C_{10}H_8N_2, 98\%$ , Aldrich), 4-(2-pyridin-4-ylethynyl)pyridine  $(C_{12}H_8N_2, 98\%$ , Chemsoon), pyrazine  $(C_4H_4N_2, 99\%$ , Aldrich), methanol (CH<sub>3</sub>OH, anhydrous, 99%, Sigma-Aldrich), ethylene glycol  $(C_2H_6O_2,$  anhydrous, 99%, Sigma-Aldrich), were purchased and used without further purification.

 $N_2$  (99.999%),  $CO_2$  (99%),  $CH_4$  (99.99%), He (99.999%), SO<sub>2</sub> (99.99%) and mixed gases of (1)  $SO_2/N_2 = 0.2/99.8$  (v/v), (2)  $SO_2/N_2 = 1/99$  (v/v), (3)  $SO_2/N_2 = 5/95$  (v/v), (4)  $SO_2/N_2 =$ 10/90 (v/v) were purchased form JinGong Company (China). Mixed gases of (5)  $SO_2/CO_2$  = 0.2/99.8 (v/v) were purchased from Shanghai Wetry Standard Reference Gas Analytical Technology Co. LTD (China).

#### *Synthesis*

Synthesis of SIFSIX-1-Cu (Cu(4,4'-bipyridine)<sub>2</sub>SiF<sub>6</sub>•8H<sub>2</sub>O)n

Firstly, 4,4'-bipyridine (0.35 g) was dissolved in ethylene glycol (40 mL) at 338 K. An aqueous solution (20 mL) of Cu(BF<sub>4</sub>)<sub>2</sub>•xH<sub>2</sub>O (266 mg, 1.12 mmol) and (NH<sub>4</sub>)<sub>2</sub>SiF<sub>6</sub> (199 mg, 1.12 mmol) was added to the above solution. Then the mixture was heated at 65 °C for 3 h under stirring. The obtained purple powder was filtered, washed with methanol, and was exchanged with methanol for 3 days.<sup>[1]</sup>

Synthesis of SIFSIX-2-Cu (Cu(4,4'-bipyridylacetylene)<sub>2</sub>SiF<sub>6</sub>)n

An ethanol solution (2.0 mL) of 4,4'-bipyridylacetylene (0.115mmol) was carefully layered onto an ethylene glycol solution  $(2.0 \text{ mL})$  of  $\text{CuSiF}_6 \cdot \text{xH}_2\text{O}$   $(0.149 \text{ mmol})$ . Crystals of SIFSIX-2-Cu were obtained after two weeks. The obtained sample was exchanged with ethanol for 4 days.[2]

Synthesis of SIFSIX-2-Cu-i (Cu(4,4'-bipyridylacetylene)<sub>2</sub>SiF<sub>6</sub>).

A methanol solution (4.0 mL) of 4,4'-bipyridylacetylene (0.286 mmol) was mixed with an aqueous solution (4.0 mL) of Cu(BF<sub>4</sub>)<sub>2</sub>•xH<sub>2</sub>O (0.26 mmol) and (NH<sub>4</sub>)<sub>2</sub>SiF<sub>6</sub> (0.26 mmol) and then heated at 85 °C for 12 h. The obtained sample was exchanged with methanol for 3 days. [2]

#### Synthesis of SIFSIX-3-Zn  $(Zn(pyrazine)_2SiF_6)n$

A methanol solution (2.0 mL) of pyrazine (1.3mmol) was carefully layered onto a methanol solution (2.0 mL) of  $ZnSiF_6\bullet xH_2O$  (0.13 mmol). Colourless crystals of SIFSIX-3-Zn were obtained after two days. The obtained sample was exchanged with ethanol for 1 days.<sup>[2]</sup> Synthesis of SIFSIX-3-Ni (Ni(pyrazine)<sub>2</sub>SiF<sub>6</sub>)n

A methanol solution (20 ml) of nickel silicofluoride,  $NiSiF<sub>6</sub>$  (1mmol) and pyrazine (2mmol) was mixed and heated at 85 °C. Blue powder was obtioned after 3days. The obtained sample was exchanged with ethanol for 3 days.  $[3]$ 

#### *Pure gas adsorption*

SIFSIX-1-Cu, SIFSIX-2-Cu, SIFSIX-2-Cu-i, and SIFSIX-3-Zn were evacuated at 303 K for 1-2 days until the pressure dropped below 7μm Hg. SIFSIX-3-Ni was degased at 105 °C for 15 h under dynamic pressure below 5  $\mu$ m Hg. N<sub>2</sub>, CO<sub>2</sub> and CH<sub>4</sub> sorption isotherms were collected at 298 K on activated SIFSIX-1-Cu, SIFSIX-2-Cu, SIDSIX-2-Cu-i, SIFSIX-3-Ni and SIFSIX-3-Zn using ASAP 2050 Analyzer (Micromeritics).

#### *SO<sup>2</sup> adsorption*

 $SO<sub>2</sub>$  adsorption isotherms at 298 K and 273 K were collected using the apparatus in Figure S1. Activated samples were packed in a glass container which was partly immersed in a water bath. The  $SO_2$  adsorption isotherms were determined using  $SO_2/N_2$  mixed gas with varying  $SO<sub>2</sub>$  molar fractions under flow mode. Note: the adsorption of  $SO<sub>2</sub>$  at 1.0 atm was measured with pure  $SO<sub>2</sub>$  at flow mode. At the beginning of this experiment, the activated sample was loaded in the glass container which was full of pure  $N_2$  atmosphere at 760 mmHg. Then the  $SO_2/N_2$  mixed gas (e.g. 0.002/99.998) was introduced at a constant flow at 760 mmHg.

Adsorption equilibrium was reached until the weight of glass container kept constant and didn't change. The  $SO<sub>2</sub>$  uptake was calculated based on the weight-change before and after dynamic adsorption. This method will underestimate the  $SO<sub>2</sub>$  uptake because the samples were pre-saturated by  $N_2$  but some of  $N_2$  molecules were displaced by the  $SO_2$  molecules. At the adsorption with high  $SO_2$  molar fraction, the weight of unabsorbed  $SO_2$  gases in the glass container was subtracted by blank test.

The detailed adsorption procedures: firstly,  $SO_2/N_2$  (0.002/0.998) mixed gas was introduced into the glass container at a rate of 20 ml min<sup>-1</sup>. Equilibrium were reached until the weight of glass container kept constant and didn't change. The amount of adsorbed  $SO<sub>2</sub>$  at the partial pressure of 0.002 was determined by the electronic balance with  $\pm$  0.1 mg accuracy. Then, the uptake capacity of  $SO_2$  at the partial pressure of 0.01, 0.05, 0.1 was measured using  $SO_2/N_2$ (0.01/0.99),  $SO_2/N_2$  (0.05/0.95),  $SO_2/N_2$  (0.1/0.9) mixed gas using the repeated procedures. The higher partial pressure of  $SO<sub>2</sub>$  (e.g. 0.4, 0.5, 0.8 1.0) was controlled by changing the flow rate of  $SO_2$  and  $N_2$ .



1. Mass flow controller 2. 3-Way valve 3. Glass container 4. Water bath **Figure S1** Schematic illustration of the apparatus for the SO<sub>2</sub> adsorption experiments.

#### *Breakthrough tests*

The breakthrough experiments were carried out in a dynamic gas breakthrough equipment (fig. S2). [4] All experiments were conducted using a stainless steel column (4.6 mm inner diameter  $\times$  50 mm). According to the different particle size and density of the sample powder, the weight packed in the column was: SIFSIX-1-Cu powder (0.21 g), SIFSIX-2-Cu-i (0.21 g), and SIFSIX-3-Ni (0.50 g), respectively. The column packed with sample was firstly purged with He flow (15 ml min<sup>-1</sup>) for 12 h at room temperature (25 °C). The mixed gas of  $SO_2/N_2$  = 0.2/99.8 (v/v) was then introduced at 21 ml min<sup>-1</sup>, and  $SO_2/CO_2 = 0.2/99.8$  (v/v) ) was introduced at 14 ml min<sup>-1</sup>. Outlet gas from the column was monitored using gas chromatography (GC-2010 plus) with a thermal conductivity detector (TCD) coupled with a FID. The gas mixture was separated by a capillary column (Agilent GS-GASPRO,  $\Phi$ 0.32  $\times$ 60 M). The concentration of  $SO_2$ ,  $CO_2$  or  $N_2$  in the outlet gas was monitored by the TCD. After the breakthrough experiment, the sample was regenerated with He flow (7 to 15 ml min- $<sup>1</sup>$ ) for 6 to 20 hours.</sup>



**Figure S2** Schematic illustration of the apparatus for the breakthrough experiments.

#### *X-ray diffraction structure analysis*

Powder X-ray diffraction patterns were collected using SHIMADZU XRD-6000 diffractometer (Cu K<sub>a</sub>  $\lambda$  = 1.540598 Å) with an operating power of 40 Kv and fixed divergence slit of 0.76 mm. The data were collected in the range of  $2\theta = 3-50^{\circ}$ .

Powder X-ray diffraction patterns of bare and SO<sub>2</sub>-loaded SIFSIX-1-Cu and SIFSIX-2-Cu-i were collected using PANalytical X'Pert Pro diffractometer (Cu K<sub> $\alpha$ </sub>  $\lambda$  = 1.540598 Å) with an operating power of 40 Kv and fixed divergence slit of 0.380 mm. The data were collected in the range of  $2\theta = 3-60^{\circ}$ .

#### *Density-functional theory calculations*

First-principles density-functional theory (DFT) calculations were performed using the Quantum-Espresso package. A semi-empirical addition of dispersive forces to conventional DFT was included in the calculation to account for van der Waals interactions.<sup>[5]</sup> We used Vanderbilt-type ultrasoft pseudopotentials and generalized gradient approximation (GGA) with Perdew-Burke-Ernzerhof (PBE) exchange correlation. A cutoff energy of 544 Ev and a  $2\times2\times4$  k-point mesh (generated using the Monkhosrt-Pack scheme) were found to be enough for the total energy to converge within  $0.01$  meV atom<sup>-1</sup>. We first optimized the structure of SIFSIX MOFs. The optimized structures are good matches for the experimentally determined crystal structures of the coordination networks. Various guest gas molecules were then introduced to to various locations of the channel pore, followed by a full structural relaxation. To obtain the gas binding energy, an isolated gas molecule placed in a supercell (with the same cell dimensions as the MOF crystal) was also relaxed as a reference. The static binding energy (at  $T = 0$  K) was then calculated using:  $EB = E(MOF) + E(gas) - E(MOF + gas)$ .

#### *Fitting of isotherms*

The isotherm data for  $SO_2$ ,  $CO_2$ ,  $CH_4$ , and  $N_2$  in SIFSIX-1-Cu, SIFSIX-2-Cu-i, SIFSIX-3-Zn, and SIFSIX-3-Ni were fitted with either the Langmuir-Freundlich isotherm model.

$$
q = q_{sat} \frac{bp^{\nu}}{1 + bp^{\nu}}
$$
 (1)

with *T*-dependent parameters *b*

$$
b = b_0 \exp\left(\frac{E}{RT}\right) \tag{2}
$$

The fitted parameter values are presented in Table S1

Notation



#### *Isosteric heat of adsorption*

The binding energy of SO<sub>2</sub> is reflected in the isosteric heat of adsorption,  $Q_{st}$ , defined as

$$
Q_{st} = RT^2 \left(\frac{\partial \ln p}{\partial T}\right)_q \tag{3}
$$

Figure S3 presents a comparison of the heats of adsorption of  $SO<sub>2</sub>$  in various SIFSIX; the calculations are based on the use of the Clausius-Clapeyron equation.

#### *IAST claculations of adsorption selectivities*

The adsorption selectivity for  $C_2H_2/C_2H_4$  separation is defined by

$$
S_{ads} = \frac{q_1/q_2}{p_1/p_2} \tag{3}
$$

*q*1, and *q*<sup>2</sup> are the molar loadings in the adsorbed phase in equilibrium with the bulk gas phase with partial pressures *p*1, and *p*2.

**Table S1.** Langmuir-Freundlich parameter fits for  $SO_2$ ,  $CO_2$ ,  $CH_4$ , and  $N_2$  in SIFSIX materials. The isotherm data for CH<sub>4</sub>, and  $N_2$  were only measured at 298 K, and therefore  $E =$ 0.

		SIFSIX-1-Cu		
		$\mathcal{D}_0$		
	$q_{\text{sat}}$ mol kg <sup>-1</sup>	$Pa^{-\nu_i}$	$kJ \text{ mol}^{-1}$	dimensionless
SO <sub>2</sub>	l 17	$9.8 \times 10^{-8}$	26	0.72
CO <sub>2</sub>	12	$1.12\times10^{-13}$	33	1.2
CH4	12	$3.9 \times 10^{-7}$	0	
N,	12	$1.54 \times 10^{-7}$	O	



SIFSIX-3-Ni *q*sat  $\text{mol} \text{kg}^{-1}$  $b_0$  $Pa^{-\nu_i}$ *E* kJ $\mathrm{mol}^{\text{-}1}$ *ν*  $\frac{\text{dimensionless}}{1.07}$  $SO<sub>2</sub>$ 2.7  $3.05 \times 10^{-11}$  46.2 CH<sup>4</sup> 12  $3.9 \times 10^{-7}$  0 1  $\rm N_2$ 12  $2.08 \times 10^{-7}$  0 1



**Table S2.** The volumetric uptake of  $SO<sub>2</sub>$  (density per crystal cell volume) in various SIFSIX materials at 1.01 bar.









2 Theta	h	k	$\mathbf{l}$	d-
				spacing
7.934	$\mathbf{1}$	$\boldsymbol{0}$	$\boldsymbol{0}$	11.1348
11.044	$\overline{0}$	$\boldsymbol{0}$	$\mathbf{1}$	8.00474
11.229	1	$\mathbf{1}$	$\boldsymbol{0}$	7.87352
13.613	1	$\overline{0}$	$\mathbf{1}$	6.49954
15.775	1	$\mathbf{1}$	$\mathbf{1}$	5.61324
15.906	$\overline{c}$	$\boldsymbol{0}$	$\boldsymbol{0}$	5.56742
17.798	$\overline{c}$	$\mathbf{1}$	$\boldsymbol{0}$	4.97965
19.406	$\overline{c}$	$\boldsymbol{0}$	$\mathbf{1}$	4.57062
20.993	$\overline{c}$	$\mathbf{1}$	$\mathbf{1}$	4.22826
22.193	$\overline{0}$	$\boldsymbol{0}$	$\overline{c}$	4.00237
22.568	$\overline{c}$	$\overline{c}$	$\boldsymbol{0}$	3.93676
22.602	$\mathbf{1}$	$\overline{0}$	$\overline{c}$	3.76645
23.956	3	$\boldsymbol{0}$	$\overline{0}$	3.71162
24.937	$\mathbf{1}$	$\mathbf{1}$	$\overline{c}$	3.56786
25.189	$\overline{c}$	$\overline{c}$	$\mathbf{1}$	3.53265
25.273	3	$\mathbf{1}$	$\boldsymbol{0}$	3.52115
26.448	$\overline{\mathbf{3}}$	$\overline{0}$	$\mathbf{1}$	3.36725
27.423		$\boldsymbol{0}$	$\overline{c}$	3.24977
27.654	$\frac{2}{3}$	$\mathbf{1}$	$\mathbf{1}$	3.2231
28.591	$\overline{c}$	$\mathbf{1}$	$\overline{c}$	3.11962
28.887	$\overline{3}$	$\overline{c}$	$\boldsymbol{0}$	3.08825
31.013	3	$\overline{c}$	$\mathbf{1}$	2.88126
31.859	$\overline{2}$	$\overline{2}$	$\overline{2}$	2.80662
32.129	$\overline{4}$	$\overline{0}$	$\boldsymbol{0}$	2.78371
32.884	3	$\boldsymbol{0}$	$\overline{c}$	2.7215
33.146	4	$\mathbf{1}$	$\boldsymbol{0}$	2.7006
33.559	$\boldsymbol{0}$	$\boldsymbol{0}$	$\overline{\mathbf{3}}$	2.66825
33.880	3	$\mathbf{1}$	$\overline{c}$	2.64368
34.072	4	$\overline{0}$	$\overline{1}$	2.62926
34.136	3	3	$\overline{0}$	2.62451
34.539	$\mathbf{1}$	$\boldsymbol{0}$	3	2.59479
35.039	4	$\mathbf{1}$	$\mathbf{1}$	2.55889
35.494	$\mathbf{1}$	$\mathbf{1}$	$\overline{\mathbf{3}}$	2.52708
35.983	3	3	$\mathbf{1}$	2.49389
36.044	$\overline{4}$	$\overline{c}$	$\boldsymbol{0}$	2.48983
36.728	$\overline{\mathbf{3}}$	$\overline{2}$	$\overline{c}$	2.44501
37.342	$\overline{c}$	$\boldsymbol{0}$	$\overline{\mathbf{3}}$	2.40618
37.810	4	$\overline{c}$	$\mathbf{1}$	2.37747
38.237	$\overline{c}$	$\mathbf{1}$	3	2.35189
39.396	4	$\overline{0}$	$\overline{c}$	2.28531
40.253	4	$\mathbf{1}$	$\overline{2}$	2.23865
40.473	5	$\boldsymbol{0}$	$\boldsymbol{0}$	2.22697
40.473	4	3	$\boldsymbol{0}$	2.22697
40.822	$\overline{2}$	$\overline{c}$	$\overline{\mathbf{3}}$	2.20873
41.094	3	$\overline{\mathbf{3}}$	$\overline{c}$	2.19473
41.311	5	$\mathbf{1}$	$\overline{0}$	2.18372
41.654	$\overline{3}$	$\overline{0}$	$\overline{\mathbf{3}}$	2.16651

Table S4. List of Miller Index of the simulated pattern of SIFSIX-1-Cu•SO<sub>2</sub>









2 Theta	h	k	$\mathbf{l}$	d-spacing
9.101	$\mathbf{1}$	$\mathbf{1}$	$\boldsymbol{0}$	9.70963
12.552	$\mathbf{1}$	$\boldsymbol{0}$	$\mathbf{1}$	7.04657
12.884	$\overline{c}$	$\boldsymbol{0}$	$\boldsymbol{0}$	6.86575
18.024	$\overline{c}$	$\mathbf{1}$	$\mathbf{1}$	4.9175
18.259	$\overline{c}$	$\overline{c}$	$\overline{0}$	4.85482
20.436	$\overline{3}$	$\mathbf{1}$	$\boldsymbol{0}$	4.34228
21.631	$\boldsymbol{0}$	$\boldsymbol{0}$	$\overline{c}$	4.10502
22.218	3	$\boldsymbol{0}$	$\mathbf{1}$	3.99784
23.510	$\mathbf{1}$	$\mathbf{1}$	$\overline{c}$	3.78099
25.257	$\overline{c}$	$\boldsymbol{0}$	$\overline{c}$	3.52329
25.766	$\overline{3}$	$\overline{c}$	$\mathbf{1}$	3.45482
25.934	$\overline{4}$	$\boldsymbol{0}$	$\boldsymbol{0}$	3.43287
27.537	3	3	$\boldsymbol{0}$	3.23654
28.451	$\overline{c}$	$\overline{c}$	$\overline{2}$	3.13464
28.908	$\overline{4}$	$\mathbf{1}$	$\mathbf{1}$	3.08613
29.059	$\overline{4}$	$\overline{2}$	$\boldsymbol{0}$	3.07046
29.930	3	$\mathbf{1}$	$\overline{2}$	2.98304
33.242	5	$\mathbf{1}$	$\boldsymbol{0}$	2.69297
	$\mathbf{1}$			
33.358		$\boldsymbol{0}$	$\mathfrak{Z}$	2.6839
34.017	$\overline{4}$	$\boldsymbol{0}$	$\overline{c}$	2.63341
34.407	$\overline{4}$	3	$\mathbf{1}$	2.60445
34.407	5	$\boldsymbol{0}$	$\mathbf{1}$	2.60445
35.285	3	3	$\overline{c}$	2.54159
35.897	$\overline{c}$	$\mathbf{1}$	$\overline{\mathbf{3}}$	2.49969
36.515	$\overline{4}$	$\overline{c}$	$\overline{c}$	2.45875
36.882	5	$\overline{c}$	$\mathbf{1}$	2.43513
37.004	$\overline{4}$	$\overline{4}$	$\boldsymbol{0}$	2.42741
38.186	5	3	$\boldsymbol{0}$	2.35493
38.288	$\overline{\mathbf{3}}$	$\overline{0}$	$\mathfrak{Z}$	2.34886
39.338	6	$\boldsymbol{0}$	$\overline{0}$	2.28858
40.010	5	1	$\overline{c}$	2.25169
40.560	3	2	3	2.2224
41.451	6	$\mathbf{1}$	$\mathbf{1}$	2.17666
41.561	6	$\overline{c}$	$\boldsymbol{0}$	2.17114
42.731	$\overline{4}$	$\mathbf{1}$	$\mathfrak{Z}$	2.11439
43.266	$\overline{4}$	$\overline{4}$	$\overline{2}$	2.08944
43.585	5	$\overline{4}$	$\mathbf{1}$	2.07488
44.085	$\boldsymbol{0}$	$\boldsymbol{0}$	$\overline{4}$	2.05251
44.309	5	3	$\overline{2}$	2.04268
45.112	$\mathbf{1}$	$\mathbf{1}$	$\overline{4}$	2.00813
45.332	6	$\boldsymbol{0}$	$\overline{c}$	1.99892
45.639	6	3	$\mathbf{1}$	1.98617
46122	$\overline{c}$	$\boldsymbol{0}$	$\overline{4}$	1.96652
46.740	$\overline{7}$	$\mathbf{1}$	$\boldsymbol{0}$	1.94193
46.740	5	5	$\boldsymbol{0}$	1.94193
46.827	4	3	$\overline{3}$	1.93852
46.827	5	$\boldsymbol{0}$	$\overline{3}$	1.93852

Table S6. List of Miller Index of the simulated pattern of SIFSIX-2-Cu-i•SO<sub>2</sub>





Figure S3 Comparison of  $Q_{st}$  of SO<sub>2</sub> adsorption in SIFSIX materials.



Figure S4 Adsorption isotherms for SO<sub>2</sub>, CO<sub>2</sub> and CH<sub>4</sub> on SIFSIX-3-Zn at 298 K and 1.0 bar. Note: the adsorption isotherm of  $SO_2$  were determined using  $SO_2/N_2$  mixed gas with varying SO<sup>2</sup> molar fractions under flow mode.



Figure S5 IAST selectivities of SO<sub>2</sub>/CH<sub>4</sub> on SIFSIX materials with varying SO<sub>2</sub> molar fractions in gas phase at 100 kPa.



**Figure S6.** PXRD patterns of sample SIFSIX-2-Cu-i (A), SIFSIX-1-Cu (B), SIFSIX-3-Zn (C) and SIFSIX-3-Ni (D).



Figure S7 Schematic pictures from DFT-D simulation reveal the SO<sub>2</sub> adsorbed at the secondary adsorption sites of SIFSIX-1-Cu through diploe-diploe interactions. (Note: the secondary adsorbed SO<sub>2</sub> molecules were highlighted with bright colour).



Figure S8 DFT-D simulated optimized SO<sub>2</sub> adsorption sites of SIFSIX-2-Cu in two different viewing directions (A and B).



Figure S9 DFT-D simulated optimized SO<sub>2</sub> adsorption sites of SIFSIX-3-Zn viewed down the *c* axis.



**Figure S10.** DFT-D calculated CO<sub>2</sub> adsorption sites in SIFISX-2-Cu-i viewing in two different directions (A and B). (Note: the different nets are highlighted in magenta and cyan for clarity).

As shown in Figure S10,  $CO<sub>2</sub>$  were trapped in the interpenetrated SIFSIX-2-Cu-i through  $C^{\delta^+}\cdots F^{\delta^-}$  and multiple  $O^{\delta^-}\cdots H^{\delta^+}$  interactions. The DFT-D calculated distance of  $C\cdots F$  from different nets are 2.80 and 2.52 Å, respectively (Figure S10). By contrast, the DFT-D calculated distance of  $S \cdots F$  from different nets are both 2.44 Å, indicating much stronger electrostaic interactions between  $SO_2$  and SIFSIX-2-Cu-i.



**Figure S11.** DFT-D calculated  $CO<sub>2</sub>$  binding sites in SIFSIX-1-Cu viewing in two different directions (A and B). Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Cu, dark teal; O, orange.

In SIFSIX-1-Cu, the adsorbed  $CO_2$  are bound by the  $C^{\delta^+} \cdots F^{\delta^-}$  (Figure S11A) and multiple  $O^{\delta}$  ···· H<sup> $\delta$ +</sup> (Figure S11B) interactions. The DFT-D calculated distance of C··· F (2.60 Å) is comparable to the calculated distance of  $S^{\cdots}F$  is 2.61 Å. And the DFT-D calculated  $O^{\cdots}H$ distance of  $CO_2$  molecule with 4,4'-bipyridine ranged form 2.64  $\sim$  3.58 Å, longer than the O…H distance of SO<sub>2</sub> molecule with  $4.4$ <sup>2</sup>-bipyridine  $(2.39~3.30 \text{ Å})$ . These multiple interactions shows a stronger interactions between  $SO_2$  and SIFSIX-1-Cu.



Figure S12. DFT-D calculated  $CO<sub>2</sub>$  binding sites in SIFSIX-3-Zn. Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Zn, violet; O, orange.

With a samll pore size of SIFSIX-3-Zn,  $CO<sub>2</sub>$  were captured through four cooperative  $C^{\delta^+}\cdots F^{\delta^-}$  and multiple  $O^{\delta^-}\cdots H^{\delta^+}$  interactions. Adsorbed at the center of the one-dimensional channel (Figure S12), all of the four C···F distance were 3.36 Å.



**Figure S13**. DFT-D calculated  $N_2$  adsorption sites in SIFSIX-1-Cu (A), SIFSIX-3-Zn (B), and SIFISX-2-Cu-i (C). Colour code: F, red; Si, light blue; C, grey; H, light grey; N, sky blue; Cu, dark teal; Zn, violet; O, orange. (Note: the different nets of SIFSIX-2-Cu-i are highlighted in magenta and cyan for clarity).

In addition, the calculated adsorption energy  $(\Delta E)$  shows that there are much stronger interactions with SO<sub>2</sub> than CO<sub>2</sub> ( $\Delta E$  in SIFSIX-2-Cu-i, 50.2 versus 35.7 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-1-Cu, 50.3 versus 31.1 kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-3-Zn, 54.1 versus 45.7 kJ mol<sup>-1</sup>). As for N<sub>2</sub>, the calculated  $\Delta E$  also shows that there are much stronger interactions with SO<sub>2</sub> than  $N_2$  (Δ*E* in SIFSIX-2-Cu-i, 50.2 versus 22.8 kJ mol<sup>-1</sup>; Δ*E* in SIFSIX-1-Cu, 50.3 versus 15.7kJ mol<sup>-1</sup>;  $\Delta E$  in SIFSIX-3-Zn, 54.1 versus 25.2 kJ mol<sup>-1</sup>).



Figure S14. Powder X-ray diffraction patterns for the Rietveld refinement of SO<sub>2</sub>-loaded SIFSIX-1-Cu (A) and SO<sub>2</sub>-loaded SIFSIX-2-Cu-i (B). Goodness of fit data: (A)  $R_{wp} = 0.0891$ ,  $R_p= 0.0624$ ,  $\chi^2 = 3.96$ ; (B)  $R_{wp} = 0.0666$ ,  $R_p = 0.0492$ ,  $\chi^2 = 1.99$ .



**Figure S15.** TGA patterns of sample SIFSIX-3-Zn and SIFSIX-3-Ni (A). XRD patterns of sample SIFSIX-3-Zn (B) and SIFSIX-3-Ni (C) after exposure to 75% humidity for 1 day.



Figure S16. Experimental desorption curves for SO<sub>2</sub> on SIFSIX-2-Cu-i (Φ4.6×50 mm, 0.21 g) and SIFSIX-1-Cu ( $\Phi$ 4.6×50 mm, 0.23 g) with He flow of 20 ml min<sup>-1</sup> at 313 K.



Figure S17. Experimental column breakthrough curves for SO<sub>2</sub>/CO<sub>2</sub> separations on SIFSIX-2-Cu-i (Φ4.6×50 mm, 0.21 g) at 298 K and 1.01 bar with the presence of moisture. The composition of the mixed gas:  $1000$  ppm  $H<sub>2</sub>O$ ,  $1870$  ppm  $SO<sub>2</sub>$ , and  $99.713\%$   $CO<sub>2</sub>$ .



**Figure S18.** XRD patterns of sample SIFSIX-2-Cu-i after exposure to 75% humidity for 1 day (A). The BET curves of fresh SIFSIX-2-Cu-i and the sample after exposure to 75% humidity for 1 day (B). XRD patterns of sample SIFSIX-3-Ni after exposure to 70% humidity for 5 days (C). The BET curves of fresh SIFSIX-3-Ni and the sample after exposure to 70% humidity for 5 days (D).  $[6]$ 

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