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# Two Analogous Polyhedron-Based MOFs with High Density of Lewis Basic Sites and Open Metal Sites: Significant CO<sub>2</sub> Capture and Gas Selectivity Performance

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#### Supporting Information

**ABSTRACT:** By means of modulating the axial ligand and adopting supermolecular building blocks (SBBs) strategy, two polyhedron-based metal-organic frameworks (PMOFs) have been successfully synthesized  $[Cu_6(C_{17}O_9N_2H_8)_3(C_6H_{12}N_2)-(H_2O)_2(DMF)_2]\cdot 3DMF\cdot 8H_2O$  (JLU-Liu46) and  $[Cu_6(C_{17}O_9N_2H_8)_3(C_4H_4N_2)(H_2O)_2(DMF)_2]\cdot 3DMF\cdot 8H_2O$  (JLU-Liu47), which possess a high density of Lewis basic sites (LBSs) and open metal sites (OMSs). Since the size of axial ligand in JLU-Liu47 is smaller than that in JLU-Liu46, JLU-Liu47 shows larger pore volume and higher BET surface area. Then, the adsorption ability of JLU-Liu47 for some small



gases is better than **JLU-Liu46**. It is worthwhile to mention that both of the two compounds exhibit outstanding adsorption capability for  $CO_2$  ascribed to the introducing of urea groups. In addition, the theoretical ideal adsorbed solution theory (IAST) calculation and transient breakthrough simulation indicate that **JLU-Liu46** and **JLU-Liu47** should be potential materials for gas storage and separation, particularly for  $CO_2/N_2$ ,  $CO_2/CH_4$ , and  $C_3H_8/CH_4$  separation.

**KEYWORDS:** polyhedron metal-organic frameworks, MOP cages, porous materials,  $CO_2$  capture, gas separation

#### INTRODUCTION

The sharp increasing of  $CO_2$  in the atmosphere, produced by the burning of fossil fuels (such as coal, oil, and natural gas), has led to global warming.<sup>1–5</sup> Therefore, reducing the  $CO_2$ emissions and developing clear energy sources have become the most urgent environmental issues. Currently, promoting the  $CO_2$  capture and separation technologies will play a fatal role in dealing with the problems.

Metal–organic frameworks (MOFs), which have significant applications in gas capture, storage, and separation, are a new kind of promising advanced materials compared to the traditional porous zeolites and carbon materials.<sup>6–13</sup> Besides, metal–organic polyhedral (MOP) which owns a large-void cage and open-channel type is a prominent building unit to construct MOFs with large pore volume, high surface area, and excellent gas uptake capacity.<sup>14–17</sup> For the sake of constructing polyhedron-based metal–organic frameworks (PMOFs), a supermolecular building blocks (SBBs) approach is considered an effective strategy which has been used to configure a series of classic PMOFs, such as *rht*-MOFs,<sup>18</sup> *gea*-MOFs,<sup>19</sup> and *fcu*-MOFs.<sup>20</sup> In addition, it also indicates that the ligands, with functional groups such as amino, imino, amide, urea, imidazole, and triazole in the PMOFs may significantly improve the storage and separation performance for  $CO_2$ . Therefore, many PMOFs modified with functional groups have been reported, such as NU-100,<sup>21</sup> Cu-TPBTM,<sup>22</sup> PCN-6x series,<sup>23</sup> Cu-TDPAT,<sup>24</sup> Cu-TATAB,<sup>25</sup> HUNST-5,<sup>26</sup> and so forth. As for PCN-61 and Cu-TPBTM, although the pore size, surface area, and the number of open metal sites (OMSs) for the two MOFs are almost same, the  $CO_2$  adsorption performance is different because the functional group is  $-C \equiv C-$  in PCN-61 and -NH-CO- in Cu-TPBTM.

In terms of isophthalate moiety making it convenient to construct MOP cage, the tetracarboxylic acid ligand with two isophthalate moieties is a commendable candidate to synthesize PMOFs. However, most tetracarboxylic ligands are conditioned to assemble *nbo* topology without MOP cages, such as MOF-505,<sup>27</sup> MOF-101,<sup>28</sup> UTSA-80,<sup>29</sup> PCN-16,<sup>30</sup> NOTT-105,<sup>31</sup> and NU-135.<sup>32</sup> In our preliminary work, a ligand with both tetracarboxylic and triazole moieties has been selected to

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successfully construct two novel PMOFs materials, JLU-Liu20 and JLU-Liu21, which display significant capture capacity of  $CO_2$ <sup>33</sup> In order to improve the properties of  $CO_2$  adsorption and separation, urea groups which possesses a high density of Lewis basic sites (LBSs) have been introduced as functional group to replace the triazole moieties in the tetracarboxylic ligand and a less used ligand 5,5'-(carbonylbis(azanediyl))diisophthalic acid  $(H_4L)$  is successfully prepared. Up to now, only two MOFs (NU-601<sup>34</sup> and  $Eu_4[\tilde{L}]_3^{35}$ ) based on  $H_4L$ ligand have been reported, and neither of them possess MOP cage nor adsorption abilities. Opportunely, we have successfully prepared a PMOF  $[Cu_6(C_{17}O_9N_2H_8)_3(C_6H_{12}N_2)]$ (H<sub>2</sub>O)<sub>2</sub>(DMF)<sub>2</sub>]·3DMF·8H<sub>2</sub>O (JLU-Liu46) which is made up of three different kinds of MOP cages and possesses a high density of OMSs and LBSs. In consideration of the 1,4diazabicyclo[2.2.2]-octane (DABCO) in the framework occupies a certain amount of space, and a similar but smaller pyrazine ligand is adopted to construct the same framework. Just as we expected, another analogous PMOF  $[Cu_{6}(C_{17}O_{9}N_{2}H_{8})_{3}(C_{4}H_{4}N_{2})(H_{2}O)_{2}(DMF)_{2}]\cdot 3DMF\cdot 8H_{2}O$ (JLU-Liu47) with larger pore volume than JLU-Liu46 is successfully synthesized. Both of the compounds exhibit excellent properties in small gases adsorption (CO<sub>2</sub>, CH<sub>4</sub>,  $C_2H_6$ , and  $C_3H_8$ ), especially for  $CO_2$ . Meanwhile, the simulation method of ideal adsorbed solution theory, breakthrough, and Grand Canonical Monte Carlo Simulations are applied to evaluate the gas selective separation abilities. The simulation results indicate that both JLU-Liu46 and JLU-Liu47 are promising materials for gas capture and separation.

#### EXPERIMENTAL SECTION

**Materials and Methods.** Ligand  $H_4L$  was synthesized in accordance with the literature procedure.<sup>34</sup> The structural characterization is shown in Scheme S1 and Figure S1. <sup>1</sup>H NMR (300 MHz, DMSO- $d_6$ ,  $\delta$ , ppm) 13.24 (s, 4H), 9.64 (d, 2H), 8.34 (d, J = 1.5 Hz, 4H), 8.12 (d, J = 3 Hz, 2H).

All chemicals were purchased from chemical company and used without additional purification. Powder X-ray diffraction (PXRD) pattern were recorded on a Rigaku D/max-2550 diffractometer with Cu K $\alpha$  radiation ( $\lambda$  = 1.5418 Å). Elemental analyses (C, H, and N) were performed on a vario MICRO elementary analyzer. The thermal gravimetric analyses (TGA) were carried out on a TGA Q500 thermogravimetric analyzer with a heating rate of 10 °C min<sup>-1</sup> in air.

**Synthesis of Compounds.** Synthesis of JLU-Liu46. A mixture of  $Cu(BF_4)_2 \cdot 6H_2O$  (7.5 mg, 0.012 mmol),  $H_4L$  (2 mg, 0.005 mmol), 1,4diazabicyclo[2.2.2]-octane (DABCO) (0.1 mL, 2 g in 10 mL DMF), N,N-dimethylformamide (DMF) (1 mL), ethanol (0.5 mL),  $H_2O$  (0.5 mL), and 0.35 mL of HNO<sub>3</sub> (2.7 M in DMF) were put into a 20 mL vial; then, the vial was transferred to an oven and heated at 85 °C for 12 h. Blue crystals were gathered, washed with DMF, and air-dried (58% yield based on  $Cu(BF_4)_2 \cdot 6H_2O$ ). Elemental analysis (%) calculated for JLU-Liu46  $C_{72}H_{91}Cu_6N_{13}O_{42}$ : C, 39.45; H, 4.19; N, 8.31. Found: C, 39.93; H, 4.23; N, 8.41. The experimental and simulated PXRD patterns are identical, revealing that the assynthesized compound is obtained as the pure phase (Figure S9a).

Synthesis of JLU-Liu47. A mixture of  $Cu(BF_4)_2$ · $6H_2O$  (7.5 mg, 0.012 mmol),  $H_4L$  (3 mg, 0.0075 mmol), pyrazine (0.15 mL, 2 g in 10 mL DMF), DMF (1 mL), ethanol (0.75 mL),  $H_2O$  (0.75 mL), and 0.45 mL of HNO<sub>3</sub> (2.7 M in DMF) were added to a 20 mL vial; then, the vial was put into an oven and heated at 85 °C for 10 h. Blue crystals were collected, washed with DMF, and air-dried (54% yield based on  $Cu(BF_4)_2$ · $6H_2O$ ). Elemental analysis (%) calculated for JLU-Liu47  $C_{70}H_{83}Cu_6N_{13}O_{42}$ : C, 38.93; H, 3.87; N, 8.43. Found: C, 38.98; H, 3.91; N, 8.38. The experimental and simulated PXRD patterns are identical, revealing that the as-synthesized products are phase pure (Figure S10a).

Single Crystal X-ray Crystallography. Both the crystallographic data of JLU-Liu46 and JLU-Liu47 were recorded on a Bruker Apex II CCD diffractometer using graphite-monochromated Mo K $\alpha$  ( $\lambda$  = 0.71073 Å) radiation at 20 °C. The structures were solved by direct methods and refined by full-matrix least-squares on  $F^2$  using version 5.1.36 From the difference Fourier map, all non-hydrogen atoms were definitely found and refined anisotropically. The hydrogen atoms of the ligands were generated theoretically onto the specific atoms and refined isotropically with fixed thermal factors. As the guest molecules were highly disordered and could not be modeled properly, the diffused electron densities resulting from them were removed by the SQUEEZE routine in PLATON and the results were appended in the Supporting Information. The reported refinements are of the guestfree structures using the \*.hkp files produced on a SQUEEZE routine operations. The final formula of JLU-Liu46 and JLU-Liu47 were derived from crystallographic data combined with elemental and thermogravimetric analysis data. Crystallographic data for JLU-Liu46 and JLU-Liu47 (CCDC 1555805 and 1555806) have been deposited with Cambridge Crystallographic Data Centre. Data can be found free of charge upon request at www.ccdc.cam.ac.uk/data request/cif. Crystal data and structure refinement are summarized in Table S1. The topology analysis for JLU-Liu46 and JLU-Liu47 was calculated by using TOPOS 4.0 software.<sup>3</sup>

**Gas Adsorption Measurements.** The adsorption measurements of  $N_2$ ,  $CO_2$ ,  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$  were carried out on a Micromeritics ASAP 2020. In order to completely get rid of the guest solvent molecules, **JLU-Liu46** and **JLU-Liu47** were soaked in ethanol and replaced with absolute ethanol (12 cycles for 3 days), then activated at 95 °C for 10 h under the vacuum. The nonvolatile solvent molecules have mostly been removed during the activation process as confirmed by the TGA data (Figures S11 and S12).

#### RESULTS AND DISCUSSION

Single-crystal X-ray diffraction analysis reveals that JLU-Liu46 crystallizes in the tetragonal crystal system with P4/mnc space group. The framework is aggregated with typical copper paddlewheels and two types of organic linkers (Figure S2),  $L^{4-}$  as major linker, and the DABCO as axial ligand, respectively (Figure 1a). As illustrated in Figure 1b, JLU-Liu46 has three types of cages with large Connolly surface area.



**Figure 1.** Single-crystal structure for **JLU-Liu46** and **JLU-Liu47**: Cu paddlewheel, organic L<sup>4–</sup> ligand ,and the axial ligand DABCO (a) and pyrazine (d); three types of cage with Connolly surface areas for **JLU-Liu46** (b) and **JLU-Liu47** (e); (c) arrangement of the three kinds of cage for **JLU-Liu46** and **JLU-Liu47**.



Figure 2. (a) CO<sub>2</sub>, (b) CH<sub>4</sub>, (c) C<sub>2</sub>H<sub>6</sub>, and (d) C<sub>3</sub>H<sub>8</sub> gas absorption-desorption isotherms for JLU-Liu46 at 273 and 298 K under 1 atm.

The first kind of cage is the classical MOP-1 with cuboctahedron (*cuo*) geometry  $(M_{12}L_{24})$ , which consists of 12 copper paddlewheels and 24 L<sup>4–</sup> ligands. The second kind of cage shows truncated tetrahedron (T-T<sub>d</sub>) configuration  $(M_{12}L_6)$  with 12 copper paddlewheels, 6  $L^{4-}$  ligands, and 4 DABCO ligands. The third cage is the largest one with truncated octahedron geometry  $(T-O_h)$   $(M_{24}L_{16})$  which is constructed from 24 copper paddlewheels, 16 L<sup>4-</sup> and 8 DABCO. The internal diameters of the three kinds of cages are 31 (T-O<sub>b</sub>), 12 (*cuo*), and 10 (T-T<sub>d</sub>) Å (regardless of the van der Waals radii), respectively (Figures 1c and S5). Then, the assembling of the three different kinds of polyhedron cages leads to the formation of a 3D PMOF. Moreover, JLU-Liu46 possess multiple pore systems, the diameter of the biggest square channel is approximate to be 6.5 Å  $\times$  6.5 Å along the a axis (regardless of the van der Waals radii, Figures S3 and S4). Such cages provide a beneficial environment for better access of natural gas and the consequent host-guest interaction. From the view of topology, the Cu-paddlewheels building unit can be simplified as a square, and L<sup>4-</sup> is seen as a pair of triangle geometries. The overall framework forms a (3, 4)-connected network, and the Schläfli symbol is  $\{6^2.8^2.9^2\}^2\{6^2.8\}^4\{6^2.9\}^2\{6^3.8.10^2\}$ , which is the same as those of our previously reported JLU-Liu20 and JLU-Liu21 materials (Figure S8). The total accessible volume of JLU-Liu46 calculated by PLATON is 63.0%.

As an axial ligand, DABCO unit connects two adjacent paddlewheels and doubly supports the framework, which greatly enhances the framework rigidity and stability. However, it reduces the size of window for the framework at the same time. In order to mitigate the disadvantage, pyrazine, which has the same shape but smaller size to DABCO, is selected to synthesize another analogous PMOF. Fortunately, the presumptive PMOF JLU-Liu47 is successfully obtained, which possesses a framework similar to that of JLU-Liu46 (Figures 1c-e and S6). The structure difference between them is the axial ligand in JLU-Liu46 is DABCO, while it is pyrazine in JLU-Liu47. DABCO, with an axial length of 2.6 Å, is connected to two paddlewheels with a distance of 6.9 Å in JLU- Liu46. By contrast, the pyrazine with an axial length of 2.8 Å is linked to two paddlewheels with a distance of 7.1 Å in JLU-Liu47. Hence, the windows in JLU-Liu46 are smaller than those in JLU-Liu47 (Figure S7). Moreover, the larger transverse dimension of DABCO (4.0 Å) makes JLU-Liu46 own smaller accessible pore volumes (63.0%) than JLU-Liu47 (66.5%), which can be verified by PLATON. Therefore, the adsorption performance of JLU-Liu47 will be changed compared to JLU-Liu46.

**Thermal Stability Analyses.** The thermal stability of JLU-Liu46 and JLU-Liu47 are estimated by variable-temperature powder X-ray diffraction (VTPXRD) and thermogravimetric analysis (TGA), cooperatively. In the respect of VTPXRD, both of the compounds can keep its integrity until 200 °C (Figures S9b and 10b). From the TGA point of view, JLU-Liu46 can be steady to 250 °C, and the 42.9% weight loss is attributed to the release of guest molecules. Subsequently, the framework collapsed and displays 37.2% (calcd 36.8%) weight loss (Figure S11). Similarly, JLU-Liu47 shows 32.3% weight loss before 250 °C and a further 38.9% (calcd 37.8%) weight loss until 450 °C (Figure S12).

Gas Adsorption of JLU-Liu46 and JLU-Liu47. The reversible type I isotherm obtained by  $N_2$  adsorption measurement at 77 K verify the permanent porosities of JLU-Liu46 and JLU-Liu47 (Figure S13). The Brunauer–Emmett–Teller (BET) surface area of JLU-Liu46 is calculated to be 1787 m<sup>2</sup> g<sup>-1</sup>, and the Langmuir surface area is 2400 m<sup>2</sup> g<sup>-1</sup>. The experimental total pore volume resulted from the  $N_2$  isotherm was found to be 0.87 cm<sup>3</sup> g<sup>-1</sup>, which is pretty close to the theoretical pore volume (0.91 cm<sup>3</sup> g<sup>-1</sup>). Owing to the multiple pore systems, high density of OMSs/LBSs, and surface areas of JLU-Liu46, it also features good adsorption capacity for other small gases.

The CO<sub>2</sub> uptake of **JLU-Liu46** is determined to be 185 (36.3 wt %) and 104 (20.4 wt %) cm<sup>3</sup> g<sup>-1</sup> at 273 and 298 K under 1 atm, respectively, much higher than those of most reported MOFs materials, such as Zn-MOF-74 (17.6 wt %),<sup>38</sup> Cu<sub>3</sub>(BTC)<sub>2</sub> (18.4 wt %),<sup>39</sup> and PCN-6 (15.9 wt %).<sup>40</sup> Due to the high density of LBSs and OMSs which provide a larger



Figure 3. (a) CO<sub>2</sub>, (b) CH<sub>4</sub>, (c) C<sub>2</sub>H<sub>6</sub>, and (d) C<sub>3</sub>H<sub>8</sub> gas absorption-desorption isotherms for JLU-Liu47 at 273 and 298 K under 1 atm.



Figure 4.  $CO_2$ ,  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$  adsorption isotherms at 298 K along with the dual-site Langmuir Freundlich (DSLF) fits (a, c); Gas mixture adsorption selectivity are predicted by IAST at 298 K and 100 kPa for JLU-Liu46 (b, d).

number of force sites for CO<sub>2</sub> molecules, **JLU-Liu46** exhibits outstanding adsorption capacity of CO<sub>2</sub>. This result suggests that **JLU-Liu46** could be a good candidate for CO<sub>2</sub> capture and storage. At zero loading, the adsorption enthalpy of **JLU-Liu46** is 32 kJ mol<sup>-1</sup> (Figure S15a), higher than those of the MOFs based on Cu-paddlewheel unit and multidentate carboxylic acid ligand, such as PCN-124 (26.3),<sup>41</sup> PCN-66 (26.2),<sup>23</sup> PCN-61 (22.0),<sup>23</sup> NOTT-125 (25.4),<sup>42</sup> and NOTT-122 (24.5).<sup>43</sup> The adsorption of some other light hydrocarbons CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, and C<sub>3</sub>H<sub>8</sub> are also measured at 273 and 298 K under 1 atm, respectively. The maximum uptake for CH<sub>4</sub> is 31 and 17 cm<sup>3</sup> g<sup>-1</sup>, that for C<sub>2</sub>H<sub>6</sub> is 158 and 107 cm<sup>3</sup> g<sup>-1</sup>, and that for C<sub>3</sub>H<sub>8</sub> is 171 and 154 cm<sup>3</sup> g<sup>-1</sup>, respectively (Figure 2b–d). Furthermore,

the  $Q_{st}$  of CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, and C<sub>3</sub>H<sub>8</sub> are 15, 28, and 33 kJ mol<sup>-1</sup>, respectively (Figure S15b-d).

As far as JLU-Liu47, its BET surface areas and Langmuir surface area were calculated to be 1800 and 2493 m<sup>2</sup> g<sup>-1</sup>, respectively (Table S2). Rationally, the CO<sub>2</sub>, CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, and C<sub>3</sub>H<sub>8</sub> adsorption performance for JLU-Liu47 is better than JLU-Liu46. At 273 and 298 K, the maximum adsorption of CO<sub>2</sub> is 192 (37.7 wt %) and 108 (21.2 wt %) cm<sup>3</sup> g<sup>-1</sup> (Figure 3a). Moreover, the CO<sub>2</sub> adsorption capacity of JLU-Liu47 increases to 4.3 wt %, and that of JLU-Liu46 is 2.9 wt % at 298 K and 0.15 bar, which is pointedly higher than many reported Cu-MOFs under the same condition (Table S5). Significantly, in comparison with triazole functionalized MOF JLU-Liu20, JLU-Liu47 shows higher CO<sub>2</sub> uptake at 1 bar (Table S3, S4).

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Figure 5.  $CO_2$ ,  $CH_4$ ,  $C_2H_6$ , and  $C_3H_8$  adsorption isotherms at 298 K along with the dual-site Langmuir Freundlich (DSLF) fits (a, c); gas mixture adsorption selectivity are predicted by IAST at 298 K and 100 kPa for JLU-Liu47 (b, d).



Figure 6.  $CO_2$  and  $N_2$  adsorption isotherms at 298 K along with the dual-site Langmuir Freundlich (DSLF) fits for JLU-Liu46 (a) and JLU-Liu47 (c); gas mixture adsorption selectivity are predicted by IAST at 298 K and 100 kPa for JLU-Liu46 (b) and JLU-Liu47 (d).

The phenomenon is due to the size of pyrazine is smaller than DABCO, and JLU-Liu47 has a larger pore volume than JLU-Liu46. It is notable that the enthalpy of CO<sub>2</sub> for JLU-Liu47 reaches up to 35 kJ mol<sup>-1</sup> (Figure S16a), which is due to the high OMSs density, anionic skeletons, multiple pore systems, and higher surface area of JLU-Liu47 frameworks coordinately provide stronger interactions to the CO<sub>2</sub> molecules.

Similarly, **JLU-Liu47** has better adsorption capacity for small gas molecules than does **JLU-Liu46**. The maximum adsorption of  $CH_4$  is 36 and 21 cm<sup>3</sup> g<sup>-1</sup>, that of  $C_2H_6$  is 191 and 125 cm<sup>3</sup> g<sup>-1</sup>, and that of  $C_3H_8$  is 217 and 182 cm<sup>3</sup> g<sup>-1</sup>, respectively (Figure 3b–d). Furthermore, the  $Q_{st}$  of  $CH_4$ ,  $C_2H_6$  and  $C_3H_8$  is 16, 28, and 34 kJ mol<sup>-1</sup>, respectively (Figure S16b–d).

**Separation Behaviors of JLU-Liu46 and JLU-Liu47.** For the purpose of industrial applications, the selective separation behavior of **JLU-Liu46** and **JLU-Liu47** for  $CO_2/CH_4$ ,  $C_2H_6/$  $CH_4$ , and  $C_3H_8/CH_4$  were calculated by IAST. Subsequently, the fitting parameters are used for the prediction of multicomponent adsorption by IAST. The selectivity of  $CO_2/$  $CH_4$  (50 and 50%; 5 and 95%) is 9.8 and 6.5 for **JLU-Liu46** at 298 K and 1 atm (Figure 4a,b), which are comparable to ZIF- $8^{44}$  and some carbon materials<sup>45</sup> under the same conditions. The selectivity of  $C_2H_6$  over  $CH_4$  (50 and 50%) and that of  $C_3H_8$  over  $CH_4$  (50 and 50%) are 17 and 169 at 298 K and 1 atm, respectively (Figure 4c,d).

Besides, with respect to JLU-Liu47, the selectivity of  $CO_2$  over  $CH_4$  (50 and 50%; 5 and 95%) is 10.4 and 7.3 (Figure



Figure 7. Simulations of transient breakthrough characteristics for equimolar 4-component  $CO_2/CH_4/C_2H_6/C_3H_8$  mixture in JLU-Liu46 (a) and JLU-Liu47 (b) at 100 kPa and 298 K.



Figure 8. Density distribution of CO<sub>2</sub> molecules center-of-mass of JLU-Liu46 (a) and JLU-Liu47 (b) at 298 K and 1 bar simulated by GCMC simulation.

5a,b). As shown in Figure 5, the selectivities for equimolar binary mixtures of C<sub>2</sub>H<sub>6</sub> and CH<sub>4</sub> and of C<sub>3</sub>H<sub>8</sub> and CH<sub>4</sub> are 17 and 168 (Figure 5c,d), respectively, similar to JLU-Liu46. The selectivities of C<sub>3</sub>H<sub>8</sub> over CH<sub>4</sub> for JLU-Liu46 and JLU-Liu47 are comparable to those of some reported MOFs including LIFM-26 (50),<sup>46</sup> FJI-C1 (78.7),<sup>47</sup> UTSA-35a (80),<sup>48</sup> FIR-7aht (80),<sup>49</sup> eea-MOF-4 (136),<sup>50</sup> and eea-MOF-5 (156).<sup>50</sup> Considering the difference of polarizability and quadrupole moment between CO<sub>2</sub> and CH<sub>4</sub>, the significant separation for CH<sub>4</sub> of ILU-Liu46 and ILU-Liu47 can be mainly attributed to their multiple cage features, in which the high density of OMSs and LBSs provides more interaction force between the gas molecules and frameworks. The uptake capacity to hydrocarbons increase with the increasing of the gas polarizability  $(CH_4 = 25 \times 10^{-25}, C_2H_6 = 44 \times 10^{-25}, and C_3H_8 = 63 \times 10^{-25})$ cm<sup>3</sup>). The lowest value of  $Q_{st}$  for CH<sub>4</sub>, which is in comparison with that of  $C_2H_6$  and  $C_3H_8$ , indicates that the interaction between CH<sub>4</sub> and the adsorbent is weakest.

With regard to the application of  $CO_2$  adsorption, the high uptake is an essential factor. Besides, the selectivity is another necessary determinant for the adsorbent since  $CO_2$  always mixed with other gases in practical condition. Because the kinetic diameters of  $CO_2$  and  $N_2$  are too similar to separate, it is crucial to construct porous MOFs materials with high  $CO_2/N_2$ selectivity. We calculated the selective separation properties of  $CO_2/N_2$  for **JLU-Liu46** and **JLU-Liu47**. The selectivities of  $CO_2/N_2$  (50 and 50%; 15 and 85%; and 10 and 90%) are 39, 42, and 31 for JLU-Liu46 (Figure 6a,b) and 42, 45, and 36 for JLU-Liu47 (Figure 6c,d), respectively. The  $CO_2/N_2$  selectivities of JLU-Liu46 and JLU-Liu47 are higher than those of BUT-11(31.5),<sup>51</sup> BUT-10 (18.1),<sup>51</sup> UiO-67 (9.4),<sup>51</sup> NU-1000 (9),<sup>52</sup> and NbO-Pd-1 (33.5).<sup>53</sup>

The gas molecule selectivity of porous materials determines the performance of industrial fixed bed adsorbents. For a proper evaluation of the separation potential of JLU-Liu46 and JLU-Liu47, we test the performances of transient breakthrough using simulation methodology.<sup>54,55</sup> The following parameter values were used: length of packed bed, L = 0.3 m; voidage of packed bed,  $\varepsilon = 0.4$ ; and superficial gas velocity at inlet, u =0.04 m/s.<sup>56,57</sup> We investigate the results of breakthrough of equimolar 4-component CH<sub>4</sub>/CO<sub>2</sub>/C<sub>2</sub>H<sub>6</sub>/C<sub>3</sub>H<sub>8</sub> mixture in a fixed bed packed with JLU-Liu46 and JLU-Liu47 operated at pressure of 100 kPa and 298 K (Figure 7). The simulation results are represented in terms of a dimensionless time,  $\tau$ , defined by dividing the actual time, *t*, by the characteristic time,  $L\varepsilon/u$ . The y-axis stands for the dimensionless concentration of the components at outlet of the fixed bed adsorbent. As for both JLU-Liu46 and JLU-Liu47, the breakthrough of  $C_3H_{8}$ ,  $C_2H_{61}$  and  $CO_2$  occur much later than that of  $CH_{41}$  which indicates the stronger binding of  $C_3H_{\text{8}\text{\prime}}$   $C_2H_{\text{6}\text{\prime}}$  and  $CO_2$  as compared to that of CH<sub>4</sub>, so the selection of adsorbents should be primarily based on CO2/CH4, C2H6/CH4, and C3H8/CH4 separation performance. Although both JLU-Liu46 and JLU-Liu47 have separation performance, there are definite

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distinctions in occur time of adsorbate. Therefore, combining the theoretical IAST and breakthrough simulation verified that **JLU-Liu46** and **JLU-Liu47** are promising platforms for selective adsorption and separation of  $C_3H_8$  from the mixture of  $CO_2/CH_4/C_2H_6/C_3H_8$  hydrocarbons.

**Grand Canonical Monte Carlo Simulation.** The density distribution of center-of-mass of  $CO_2$  molecules in JLU-Liu46 and JLU-Liu47 structures were simulated by Grand Canonical Monte Carlo (GCMC) method at 298 K and 1 bar.<sup>58</sup> As shown in Figure 8, it reveals that  $CO_2$  molecules in JLU-Liu46 and JLU-Liu47 mainly adhere to the cages, which may have strong overlapping potentials. As for the whole structure, the  $CO_2$  molecules are apt to locate in both the open Cu metal sites and –NHCONH– groups (Figure S17). Moreover, the density of  $CO_2$  molecules in JLU-Liu46 (Figure 8a). These results verify that the design and construction of MOFs frameworks by using polyhedron cages with more OMSs and LBSs sites would significantly enhance the  $CO_2$  adsorption.

#### CONCLUSIONS

Two analogous PMOFs (JLU-Liu46 and JLU-Liu47) have been designed and synthesized by utilizing the SBBs strategy. JLU-Liu47 exhibits higher surface area and pore volume than does JLU-Liu46 via altering the axial ligand. Benefiting from the introducing of classical Cu-paddlewheel and urea group, which provide high density of OMSs and LBSs, the two PMOFs approach high performance for CO<sub>2</sub> capture. Meanwhile, both of the two PMOFs materials display prominent adsorption selectivity for CO<sub>2</sub>/CH<sub>4</sub> and C<sub>3</sub>H<sub>8</sub>/CH<sub>4</sub>. We also point out that the synthesis strategy adopted in this work is expected to be broadly employed in the fields of constructing MOFs materials with significant CO<sub>2</sub> capture and gas selectivity performance for the efficient and practical applications.

#### ASSOCIATED CONTENT

#### **Supporting Information**

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acsami.7b10795.

PXRD, TGA, additional structural figures, and gas sorption data (PDF) Crystallographic data for JLU-Liu46 (CIF) Crystallographic data for JLU-Liu47 (CIF)

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Notes

The authors declare no competing financial interest.

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# **Supporting Information**

# Two Analogous Polyhedron-Based MOFs with High Density of

Lewis Basic Sites and Open Metal Sites: Significant CO<sub>2</sub>

## **Capture and Gas Selectivity Performance**

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Scheme for the Synthesis of H<sub>4</sub>L:



Fig. S1. H NMR spectra of H<sub>4</sub>L recorded in DMSO.



**Fig. S2.** 5, 5'-(carbonylbis(azanediyl)) diisophthalic acid ligands with different dihedral angles in **JLU-Liu46** (a, b) and **JLU-Liu47** (c, d).



**Fig. S3.** Space-filling view of the structure of **JLU-Liu46** showing multiple pores in directions of (110) (a), (101) (b), (011) (c) (regardless of van der Waals radii).



**Fig. S4.** Space-filling view of the structure of **JLU-Liu47** showing multiple pores in directions of (110) (a), (101) (b), (011) (c) (regardless of van der Waals radii).



**Fig. S5.** View of three different cages in **JLU-Liu46** (cuboctahedron = cuo-*Oh* (bule) (a), truncated tetrahedron = T-Td (yellow) (b) and truncated octahedron = T-Oh (pink)) (c).



**Fig. S6.** View of three different cages in **JLU-Liu47** (cuboctahedron = cuo-*Oh* (bule) (a), truncated tetrahedron = T-Td (green) (b) and truncated octahedron = T-Oh (orange)) (c).



**Fig. S7.** The 3D framework of **JLU-Liu46** with DABCO ligand located between two paddlewheels with the precise size (a) and **JLU-Liu47** with pyrazine ligand (b).



**Fig. S8.** Illustration of topology of **JLU-Liu46** and **JLU-Liu47**: simplification of the inorganic  $Cu_2(CO_2)_4$  (4-connected node, green) and the organic **H**<sub>4</sub>**L** linker (two 3-connected nodes, red) (a), leading to the new (3,4)-c net (b).



Fig. S9. (a) Simulated, as-synthesized and activated PXRD patterns for JLU-Liu46 samples; (b) The variable-temperature PXRD patterns for JLU-Liu46.



**Fig. S10.** (a) Simulated, as-synthesized and activated PXRD patterns for **JLU-Liu47** samples; (b) The variable-temperature PXRD patterns for **JLU-Liu47**.



Fig. S11. TGA curves of JLU-Liu46 for the as-synthesized and activated samples.



Fig. S12. TGA curves of JLU-Liu47 for the as-synthesized and activated samples.



**Fig. S13.** (a) Nitrogen sorption isotherms on **JLU-Liu46** (red) and **JLU-Liu47** (blue) at 77 K (Adsorption: closed symbols; desorption: open symbols, respectively); (b) the pore size distribution calculated using the NLDFT method.



Fig. S14. The  $N_2$  isotherm for JLU-Liu46 (a) and JLU-Liu47 (b) at 273 and 298 K under 1 bar.



Fig. S15. Isosteric heat of  $CO_2$  (a),  $CH_4$  (b),  $C_2H_6$  (c) and  $C_3H_8$  (d) for JLU-Liu46.



Fig. S16. Isosteric heat of  $CO_2$  (a),  $CH_4$  (b),  $C_2H_6$  (c) and  $C_3H_8$  (d) for JLU-Liu47.

### Calculation procedures of selectivity from IAST

The measured experimental data is excess loadings ( $q^{ex}$ ) of the pure components CO<sub>2</sub>, CH<sub>4</sub>, C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub> for **JLU-Liu46** and **JLU-Liu47**, which should be converted to absolute loadings (q) firstly.

$$q = q^{ex} + \frac{pV_{pore}}{ZRT}$$

Here Z is the compressibility factor. The Peng-Robinson equation was used to estimate the value of compressibility factor to obtain the absolute loading, while the measure pore volume  $0.85 \text{ cm}^3 \text{ g}^{-1}$  is also necessary.

The dual-site Langmuir-Freundlich equation is used for fitting the isotherm data at 298K.

$$q = q_{m_1} \times \frac{b_1 \times p^{1/n_1}}{1 + b_1 \times p^{1/n_1}} + q_{m_2} \times \frac{b_2 \times p^{1/n_2}}{1 + b_2 \times p^{1/n_2}}$$

Here *p* is the pressure of the bulk gas at equilibrium with the adsorbed phase (kPa), *q* is the adsorbed amount per mass of adsorbent (mol kg<sup>-1</sup>),  $q_{m1}$  and  $q_{m2}$  are the saturation capacities of sites 1 and 2 (mol kg<sup>-1</sup>), b<sub>1</sub> and b<sub>2</sub> are the affinity coefficients of sites 1 and 2 (1/kPa), n<sub>1</sub> and n<sub>2</sub> are the deviations from an ideal homogeneous surface.

The selectivity of preferential adsorption of component 1 over component 2 in a mixture containing 1 and 2, perhaps in the presence of other components too, can be formally defined as

$$S = \frac{q_1/q_2}{p_1/p_2}$$

 $q_1$  and  $q_2$  are the absolute component loadings of the adsorbed phase in the mixture. These component loadings are also termed the uptake capacities. We calculate the values of  $q_1$  and  $q_2$  using the Ideal Adsorbed Solution Theory (IAST) of Myers and Prausnitz.

### Transient breakthrough of mixtures in fixed bed adsorbers

The performance of industrial fixed bed adsorbers is dictated by a combination of adsorption selectivity and uptake capacity. For a proper evaluation of the separation performance, we performed transient breakthrough simulations using the simulation methodology described in the literature. For the breakthrough simulations, the following parameter values were used: length of packed bed, L = 0.3 m; voidage of packed bed,  $\varepsilon = 0.4$ ; superficial gas velocity at inlet, u = 0.04 m/s. The transient breakthrough simulation results are presented in terms of a *dimensionless* time,  $\tau$ , defined by dividing the actual time, t, by the characteristic time,  $L\varepsilon/u$ .

The data on the dimensionless gas phase concentrations at the exit, vs  $C_i/C_{i0}$  dimensionless time,  $\tau$ , are provided in the Excel data files. Notation

- $c_i$  molar concentration of species *i* in gas mixture at exit of adsorber, mol m<sup>-3</sup>.
- $c_{10}$  molar concentration of species *i* in gas mixture at inlet of adsorber, mol m<sup>-3</sup>.
- L length of packed bed adsorber, m.
- t time, s.
- u superficial gas velocity in packed bed, m s<sup>-1</sup>.

## **Grand Canonical Monte Carlo Simulations**

The density distribution of CO<sub>2</sub> molecules in the **JLU-Liu46** and **JLU-Liu47** structures were calculated through Grand Canonical Monte Carlo (GCMC) simulation at 1 bar and 298 K. The periodic boundary conditions and Universal force field (UFF) was used. The QEq method was used to equilibrate and redistribute the overall charge of atoms of CO<sub>2</sub> molecules and MOF structures. The van der Waals interactions between CO<sub>2</sub> molecules and the MOF structures were calculated using Lennard-Jones potentials. Electrostatic interaction was evaluated through Ewald summation method. The cutoff distance was set at 18.5 Å. All the GCMC simulations were carried out using the Sorption module in Material Studio software, respectively.



**Fig. S17**. Simulation snapshot for CO<sub>2</sub> molecules in the **JLU-Liu46** (a) and **JLU-Liu47** (b) framework.

Compound	JLU-Liu46	JLU-Liu47
Formula	$C_{72}H_{91}Cu_6N_{13}O_{42}$	C <sub>70</sub> H <sub>83</sub> Cu <sub>6</sub> N <sub>13</sub> O <sub>42</sub>
Formula weight	2191.82	2159.73
Temperature (K)	293(2)	293(2)
Wavelength (Å)	0.71073	0.71073
Crystal system	Tetragonal	Tetragonal
Space group	P4/mnc	P4/mnc
<i>a</i> (Å)	27.199(4)	27.397(4)
b (Å)	27.199(4)	27.397(4)
<i>c</i> (Å)	39.140(8)	38.876(8)
α (°)	90	90
β (°)	90	90
γ (°)	90	90
V (Å <sup>3</sup> )	28955(8)	29180(8)
<i>Z</i> , <i>D</i> <sub>c</sub> (Mg/m <sup>3</sup> )	8, 1.006	8, 0.983
<i>F</i> (000)	8992	8832
heta range (deg)	1.04-25.14	1.05-25.13
refins collected/unique	184506 / 13133	186518 / 13240
R <sub>int</sub>	0.0768	0.0788
data/restraints/params	13133/36/487	13240/24/473
GOF on <i>F</i> <sup>2</sup>	1.079	1.055
<i>R</i> <sub>1</sub> , <i>wR</i> <sub>2</sub> (I>2σ(I))	0.0498, 0.1572	0.0475, 0.1529
$R_1$ , $wR_2$ (all data)	0.0687, 0.1668	0.0660, 0.1591

Table S1. Crystal data and structure refinements for JLU-Liu46 andJLU-Liu47.

Compounds	SA <sub>BET</sub> (m² g⁻¹)	SA <sub>Langmuir</sub> (m² g⁻¹)	Pore volume (cm³ g⁻¹) (Experimental/Theoretical)	OMSs (nm <sup>-3</sup> )	LBSs (nm <sup>-3</sup> )
JLU-Liu46	1787	2400	0.87/0.91	1.11	1.52
JLU-Liu47	1800	2493	0.90/0.93	1.09	1.50

**Table S2.** N<sub>2</sub> adsorption data and structure information for **JLU-Liu46** and **JLU-Liu47**.

**Table S3.** Summary of CO<sub>2</sub> uptake for top MOFs reported in the literature.

Compounds	<u>CO2 Ads (wt%)</u>		Ref.	
	273K	298K		
CPM-231	45.6	N. A.	1	
Mg-MOF-74	44.7	29.4	2	
Cu-TDPAT	44.5	25.8	3	
Cu-TPBTM	42.3	23.3	4	
JLU-Liu21	41.2	23.2	5	
CPM-200Fe/Mg	40.7	24.9	6	
NJU-Bai21	40.4	22.6	7	
[Cu(Me-4py-trz-ia)]	40.5	26.8	8	
NOTT-125	40.0	18.19	9	
Nbo-pt-1	39.7	19.7	10	
LCu'	39.0	19.3	11	
SUN-5	38.5	N. A.	12	
JLU-Liu47	37.7	21.2	This work	
JLU-Liu46	36.3	20.4	This work	
JLU-Liu20	31.8	17.3	5	
PCN-88	31.4	18.4	13	
rht-MOF-7	28.7	19.3	14	
SIFXIX-2-Cu-i	28.6	23.8	15	

N.A.: Not Available. The article do not list the data.

**Table S4.** Pore characteristics and CO<sub>2</sub> adsorption data of selected MOFs based on tetracarboxylate ligand (at 1 bar).

	Surface	<u>CO<sub>2</sub> up</u>	otake (RT.	LBS	OMS	
Compounds	area	<u>wt%)</u>		(nm <sup>-1</sup> )	(nm <sup>-1</sup> )	Ref.
	(m² g⁻¹)	273K	298K			
Cu-MOF-1ª	1539	46.7	21.8	2.97	0	16
NOTT-125 <sup>b</sup>	2471	40.0	18.19	1.07	1.19	9
JLU-Liu47℃	1800	37.7	21.2	1.09	1.50	This work
JLU-Liu46°	1787	36.3	20.4	1.11	1.52	This work
HNUST-1 <sup>d</sup>	1400	30.7	18.24	0.75	0.75	17
NJU-Bai 17 <sup>e</sup>	2423	N.A.	N.A.	1.71	0.85	18
Cu(dbda) <sup>f</sup>	1516	N.A.	N.A.	1.36	1.36	19
NU-601°	N.A.	N.A.	N.A.	1.19	1.19	20
Eu₄[L]₃ <sup>c</sup>	N.A.	10.98	N.A.	1.17	0.78	21

a)-f) Ligands are corresponding with the above compounds. N.A.: Not Available. The article does not list the data.



Compounds	CO <sub>2</sub> uptake	Temperture	Ref.
	(wt%)	(K)	
mmen-Cu-BTTri	9.5	298	22
SNU-5	8.1	298	23
Cu-TDPAT	7.5	298	3
CuTATB-60	5.8	298	24
NOTT-140	5.7	298	25
PMOF-3	5.3	298	26
JLU-Liu47	4.3	298	This work
Cu-TPBTM	4.2	298	4
NJU-Bai0	4.0	298	27
HKUST-1	3.8	298	28
JLU-Liu46	2.9	298	This work
SNU-50	2.9	298	29
SNU-21S	2.25	298	30
NU-100	2.16	298	31

**Table S5**. CO2 uptake in selected Cu-MOFs at 0.15 bar.

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